

Availability

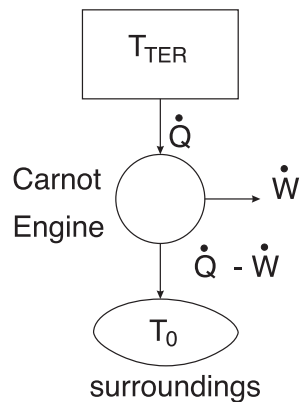
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Second Law Analysis of Systems

AVAILABILITY:

- the theoretical maximum amount of reversible work that can be obtained from a system at a given state P_1 and T_1 when interacting with a reference atmosphere at the constant pressure and temperature P_0 and T_0 .

What do we mean by work potential of a system?



Notice that:

$$\eta = \frac{\dot{W}}{\dot{Q}} = 1 - \frac{T_0}{T_{TER}}$$

Therefore

$$\dot{W} = \dot{Q} \left(1 - \frac{T_0}{T_{TER}} \right)$$

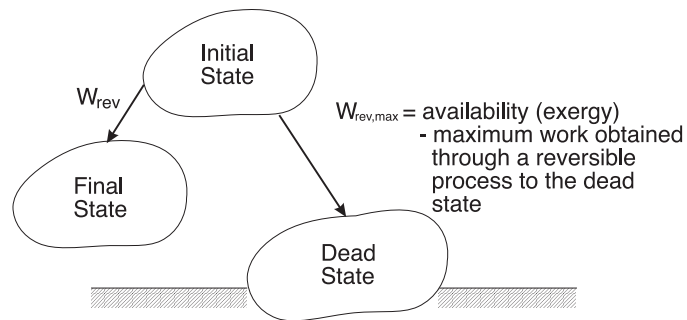
This term represents the work potential (availability) of a given TER with respect to the surroundings (dead state) at T_0 .

The following observations can be made about availability:

1. Availability is a **property** - since any quantity that is fixed when the state is fixed is a property.
2. Availability is a **composite property** - since its value depends upon an external datum
3. Availability of a system is **0** at its **dead state** when $T = T_0$ and $P = P_0$.
4. Unless otherwise stated, assume the dead state to be:

$$P_0 = 1 \text{ atm}$$

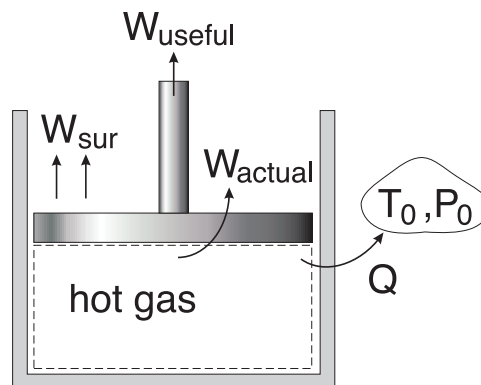
$$T_0 = 25^\circ C$$



5. The maximum work is obtained through a reversible process to the dead state.

$$\underbrace{REVERSIBLE\ WORK}_{W_{rev}} = \underbrace{USEFUL\ WORK}_{W_{useful}} + \underbrace{IRREVERSIBILITY}_I$$

Control Mass Analysis



- we know

$$W_{rev} = W_{useful} + I$$

but as shown in the figure, the actual work of the process is divided into two components

$$W_{actual} = W_{useful} + W_{sur}$$

- where W_{sur} is the part of the work done against the surroundings to displace the ambient air

$$W_{sur} = P_0(V_2 - V_1) = -P_0(V_1 - V_2)$$

To find W_{actual} , from the 1st law

$$E_1 - Q - W_{actual} = E_2 \rightarrow Q = E_1 - E_2 - W_{actual}$$

From the 2nd law

$$\begin{aligned} S_{gen} &= \Delta S_{system} + \Delta S_{sur} \geq 0 \\ &= S_2 - S_1 + \frac{Q}{T_0} \end{aligned}$$

But from the 1st law balance we know

$$\frac{Q}{T_0} = \frac{E_1 - E_2 - W_{actual}}{T_0}$$

and when we combine this with the 2nd law

$$S_{gen} = S_2 - S_1 + \frac{E_1 - E_2 - W_{actual}}{T_0}$$

which leads to

$$W_{actual} = (E_1 - E_2) + T_0(S_2 - S_1) - T_0 S_{gen}$$

or by reversing the order of S_2 and S_1

$$W_{actual} = (E_1 - E_2) - T_0(S_1 - S_2) - T_0 S_{gen}$$

But we also know that

$$W_{useful} = W_{actual} - W_{sur}$$

therefore

$$W_{useful} = (E_1 - E_2) - T_0(S_1 - S_2) + \underbrace{P_0(V_1 - V_2)}_{-W_{sur}} - T_0 S_{gen}$$

and

$$\begin{aligned} W_{rev} &= W_{useful} + I \\ &= W_{actual} - W_{sur} + I \end{aligned}$$

where

$$I = T_0 S_{gen}$$

Therefore

$$W_{rev} = (E_1 - E_2) - T_0(S_1 - S_2) + P_0(V_1 - V_2)$$

Define

$$\begin{aligned} \Phi &= \text{CONTROL MASS AVAILABILITY} \\ &= W_{rev} \text{ (in going to the dead state)} \\ &= (E - E_0) - T_0(S - S_0) + P_0(V - V_0) \end{aligned}$$

where the specific availability is defined as

$$\phi = \frac{\Phi}{m}$$

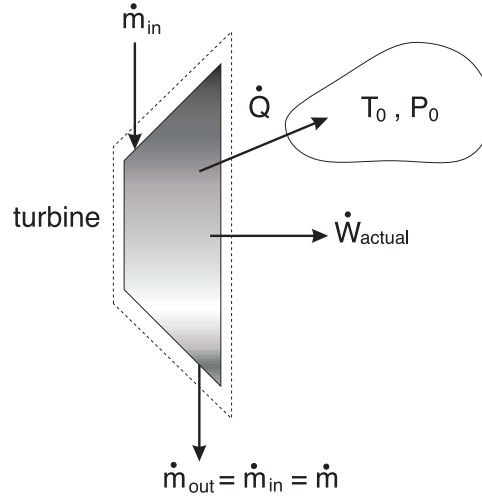
The availability destroyed is

$$I = W_{rev} - W_{useful} = T_0 S_{gen} = T_0 S_{gen}$$

This can be referred to as: irreversibilities, availability destruction or loss of availability.

Control Volume Analysis

Consider a steady state, steady flow (SS-SF) process



From the 1st law

$$\frac{dE_{cv}}{dt} = -\dot{W}_{actual} - \dot{Q} + \left[\dot{m} \left(h + \frac{(v^*)^2}{2} + gz \right) \right]_{in} - \left[\dot{m} \left(h + \frac{(v^*)^2}{2} + gz \right) \right]_{out} \quad (1)$$

From the 2nd law

$$\frac{dS_{cv}}{dt} = \left(\dot{m}s + \frac{\dot{Q}^0}{T_{TER}} \right)_{in} - \left(\dot{m}s + \frac{\dot{Q}}{T_0} \right)_{out} + \dot{S}_{gen} \quad (2)$$

Combining (1) and (2) through the \dot{Q} term, leads to the actual work output of the turbine, given as

$$\begin{aligned} \dot{W}_{actual} &= \left[\dot{m} \left(h + \frac{(v^*)^2}{2} + gz - T_0 s \right) \right]_{in} - \left[\dot{m} \left(h + \frac{(v^*)^2}{2} + gz - T_0 s \right) \right]_{out} - T_0 \dot{S}_{gen} \\ &= \dot{m} [-T_0 \Delta s + \Delta h + \Delta KE + \Delta PE] - (T_0 \dot{S}_{gen}) \end{aligned} \quad (3)$$

\dot{W}_{actual} is the actual work output of the turbine.

The specific flow availability, ψ , is given as

$$\psi = -T_0(s - s_0) + (h - h_0) + \left(\frac{(v^*)^2}{2} - \frac{(v_0^*)^2}{2} \right) + g(z - z_0) \quad (4)$$

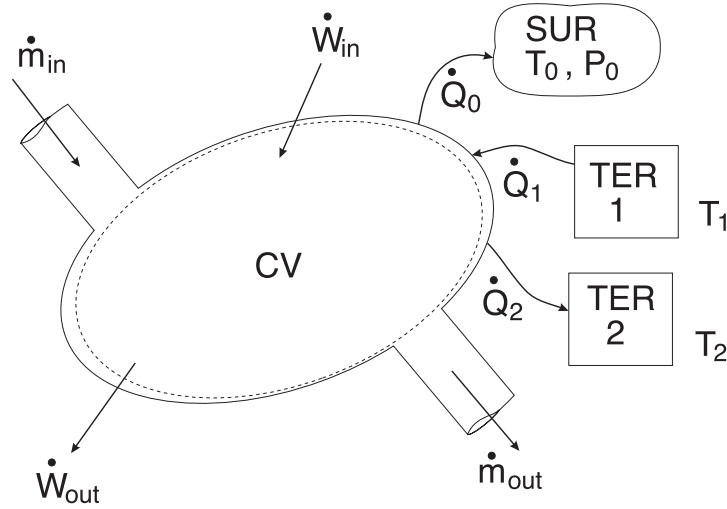
For a steady state, steady flow process where we assume KE=PE=0

$$\dot{W}_{rev} = (\dot{m}\psi)_{in} - (\dot{m}\psi)_{out} \quad (5)$$

$$\dot{I} = \dot{W}_{rev} - \dot{W}_{actual} = T_0 \dot{S}_{gen} = T_0 \dot{S}_{gen} \quad (6)$$

$$\psi = (h - h_0) - T_0(s - s_0) \quad (7)$$

The Exergy Balance Equation



From the 1st law

$$\frac{dE_{cv}}{dt} = \dot{W}_{in} - \dot{W}_{out} - \dot{Q}_0 + \dot{Q}_1 - \dot{Q}_2 + [\dot{m}(e + Pv)]_{in} - [\dot{m}(e + Pv)]_{out} \quad (1)$$

From the 2nd law

$$\frac{dS_{cv}}{dt} = \left(\dot{m}s - \frac{\dot{Q}_0}{T_0} + \frac{\dot{Q}_1}{T_1} \right)_{in} - \left(\dot{m}s + \frac{\dot{Q}_2}{T_2} \right)_{out} + \dot{S}_{gen} \quad (2)$$

Multiply (2) by T_0 and subtract from (1) to eliminate \dot{Q}_0 , which leads to the generalized exergy equation

$$\frac{d}{dt}(E - T_0 S)_{CV} = \dot{W}_{in} - \dot{W}_{out} + [\dot{m}(e + Pv - T_0 s)]_{in}$$

$$\begin{aligned}
& [\dot{m}(e + Pv - T_0s)]_{out} + \left(\dot{Q}_1 - \frac{T_0\dot{Q}_1}{T_1} \right)_{in} \\
& - \left(\dot{Q}_2 - \frac{T_0\dot{Q}_2}{T_2} \right)_{out} - T_0\dot{S}_{gen} \quad (3)
\end{aligned}$$

We can rewrite Eq. (3) in a generalized form by introducing the definitions of X and ψ .

$$\begin{aligned}
\frac{d\Phi}{dt} &= P_0 \frac{dV_{CV}}{dt} + \left[\dot{W} + \dot{m}\psi + \dot{Q} \left(1 - \frac{T_0}{T_{TER}} \right) \right]_{in} \\
&\quad - \left[\dot{W} + \dot{m}\psi + \dot{Q} \left(1 - \frac{T_0}{T_{TER}} \right) \right]_{out} - \dot{I}
\end{aligned}$$

where

$$\dot{I} = T_0\dot{S}_{gen}$$

= exergy destruction rate

$$\Phi = [(E - E_0) + P_0(V - V_0) - T_0(S - S_0)]$$

= non-flow exergy

$$\psi = (h - h_0) - T_0(s - s_0) + \frac{1}{2} [(v^*)^2 - (v_0^*)^2] + g(z - z_0)$$

= flow exergy

$$\dot{W}_{useful} = \underbrace{(\dot{W}_{in} - \dot{W}_{out})}_{\dot{W}_{actual}} - \underbrace{\left(P_0 \frac{dV_{CV}}{dt} \right)}_{W_{sur}}$$

Efficiency and Effectiveness

1. First law efficiency (thermal efficiency)

$$\eta = \frac{\text{net work output}}{\text{gross heat input}} = \frac{W_{net}}{Q_{in}}$$

Carnot cycle

$$\eta = \frac{Q_H - Q_L}{Q_H} = 1 - \frac{T_L}{T_H}$$

2. Second Law Efficiency (effectiveness)

$$\eta_{2nd} = \frac{\text{net work output}}{\text{maximum reversible work}} = \frac{\text{net work output}}{\text{availability}}$$

$$\text{Turbine} \rightarrow \eta_{2nd} = \frac{\dot{W}/\dot{m}}{\psi_e - \psi_i}$$

$$\text{Compressor} \rightarrow \eta_{2nd} = \frac{\psi_e - \psi_i}{\dot{W}/\dot{m}}$$

$$\text{Heat Source} \rightarrow \eta_{2nd} = \frac{\dot{W}/\dot{m}}{\dot{Q}/\dot{m} \left[1 - \frac{T_0}{T_{TER}} \right]}$$

3. Isentropic efficiency (process efficiency)

(a) adiabatic turbine efficiency

$$\eta_T = \frac{\text{work of actual adiabatic expansion}}{\text{work of reversible adiabatic expansion}} = \frac{W_{act}}{W_S}$$

(b) adiabatic compressor efficiency

$$\eta_C = \frac{\text{work of reversible adiabatic compression}}{\text{work of actual adiabatic compression}} = \frac{W_S}{W_{act}}$$

PROBLEM STATEMENT:

2 kg of air in a piston-cylinder device is expanded reversibly and isothermally from **700 kPa** and **250 °C** to a pressure of **125 kPa**. During the process, heat is added from a thermal energy reservoir at **250 °C**. Assume the dead state conditions to be $T_0 = 25\text{ °C}$ and $P_0 = 101.325\text{ kPa}$.

- a) Determine the amount of work transfer [***kJ***] to the piston and the amount of heat transfer [***kJ***] from the source.
- b) Determine the availability transfer [***kJ***] due to work and heat.
- c) Determine the increase in availability [***kJ***] of the air in the cylinder.
- d) Physically, how do you explain that, although the internal energy of the air did not change, its availability did?

