

**14-18** Heat generated by the electrical resistance of a bare cable is dissipated to the surrounding air. The surface temperature of the cable is to be determined.

**Assumptions** 1 Steady operating conditions exist. 2 Air is an ideal gas with constant properties. 3 The local atmospheric pressure is 1 atm. 4 The temperature of the surface of the cable is constant.

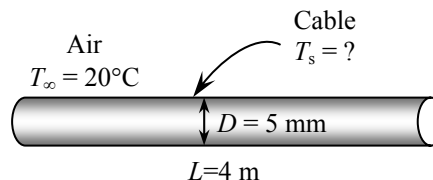
**Properties** We assume the surface temperature to be 100°C. Then the properties of air at 1 atm and the film temperature of  $(T_s + T_\infty)/2 = (100 + 20)/2 = 60^\circ\text{C}$  are (Table A-22)

$$k = 0.02808 \text{ W/m}\cdot^\circ\text{C}$$

$$\nu = 1.896 \times 10^{-5} \text{ m}^2/\text{s}$$

$$\text{Pr} = 0.7202$$

$$\beta = \frac{1}{T_f} = \frac{1}{(60 + 273)\text{K}} = 0.003003 \text{ K}^{-1}$$



**Analysis** The characteristic length in this case is the outer diameter of the pipe,  $L_c = D = 0.005 \text{ m}$ . Then,

$$Ra = \frac{g\beta(T_s - T_\infty)D^3}{\nu^2} \text{Pr} = \frac{(9.81 \text{ m/s}^2)(0.003003 \text{ K}^{-1})(100 - 20 \text{ K})(0.005 \text{ m})^3}{(1.896 \times 10^{-5} \text{ m}^2/\text{s})^2} (0.7202) = 590.2$$

$$Nu = \left\{ 0.6 + \frac{0.387 Ra^{1/6}}{\left[ 1 + (0.559 / \text{Pr})^{9/16} \right]^{8/27}} \right\}^2 = \left\{ 0.6 + \frac{0.387 (590.2)^{1/6}}{\left[ 1 + (0.559 / 0.7202)^{9/16} \right]^{8/27}} \right\}^2 = 2.346$$

$$h = \frac{k}{D} Nu = \frac{0.02808 \text{ W/m}\cdot^\circ\text{C}}{0.005 \text{ m}} (2.346) = 13.17 \text{ W/m}^2\cdot^\circ\text{C}$$

$$A_s = \pi DL = \pi (0.005 \text{ m})(4 \text{ m}) = 0.06283 \text{ m}^2$$

$$\dot{Q} = hA_s(T_s - T_\infty)$$

$$(60 \text{ V})(1.5 \text{ A}) = (13.17 \text{ W/m}^2\cdot^\circ\text{C})(0.06283 \text{ m}^2)(T_s - 20)^\circ\text{C}$$

$$T_s = 128.8^\circ\text{C}$$

which is not close to the assumed value of 100°C. Repeating calculations for an assumed surface temperature of 120°C,  $[T_f = (T_s + T_\infty)/2 = (120 + 20)/2 = 70^\circ\text{C}]$

$$k = 0.02881 \text{ W/m}\cdot^\circ\text{C}$$

$$\nu = 1.995 \times 10^{-5} \text{ m}^2/\text{s}$$

$$\text{Pr} = 0.7177$$

$$\beta = \frac{1}{T_f} = \frac{1}{(70 + 273)\text{K}} = 0.002915 \text{ K}^{-1}$$

$$Ra = \frac{g\beta(T_s - T_\infty)D^3}{\nu^2} \text{Pr} = \frac{(9.81 \text{ m/s}^2)(0.002915 \text{ K}^{-1})(120 - 20 \text{ K})(0.005 \text{ m})^3}{(1.995 \times 10^{-5} \text{ m}^2/\text{s})^2} (0.7177) = 644.6$$

$$Nu = \left\{ 0.6 + \frac{0.387 Ra^{1/6}}{\left[ 1 + (0.559 / \text{Pr})^{9/16} \right]^{8/27}} \right\}^2 = \left\{ 0.6 + \frac{0.387 (644.6)^{1/6}}{\left[ 1 + (0.559 / 0.7177)^{9/16} \right]^{8/27}} \right\}^2 = 2.387$$

$$h = \frac{k}{D} Nu = \frac{0.02881 \text{ W/m}\cdot^\circ\text{C}}{0.005 \text{ m}} (2.387) = 13.76 \text{ W/m}^2\cdot^\circ\text{C}$$

$$\dot{Q} = hA_s(T_s - T_\infty)$$

$$(60 \text{ V})(1.5 \text{ A}) = (13.76 \text{ W/m}^2\cdot^\circ\text{C})(0.06283 \text{ m}^2)(T_s - 20)^\circ\text{C}$$

$$T_s = 124.1^\circ\text{C}$$

which is sufficiently close to the assumed value of 120°C.