**6-60** Air is expanded in an adiabatic turbine. The mass flow rate of the air and the power produced are to be determined.

Assumptions 1 This is a steady-flow process since there is no change with time. 2 The turbine is well-insulated, and thus there is no heat transfer. 3 Air is an ideal gas with constant specific heats.

**Properties** The constant pressure specific heat of air at the average temperature of  $(500+150)/2=325^{\circ}C=598 \text{ K}$  is  $c_p=1.051 \text{ kJ/kg·K}$  (Table A-2b). The gas constant of air is  $R=0.287 \text{ kPa·m}^3/\text{kg·K}$  (Table A-1).

**Analysis** (a) There is only one inlet and one exit, and thus  $\dot{m}_1 = \dot{m}_2 = \dot{m}$ . We take the turbine as the system, which is a control volume since mass crosses the boundary. The energy balance for this steady-flow system can be expressed in the rate form as

$$\frac{\dot{E}_{\text{in}} - \dot{E}_{\text{out}}}{\dot{E}_{\text{in}} - \dot{E}_{\text{out}}} = \underbrace{\Delta \dot{E}_{\text{system}}^{70 \text{ (steady)}}}_{\text{Rate of net energy transfer by heat, work, and mass}} = \underbrace{\Delta \dot{E}_{\text{system}}^{20 \text{ (steady)}}}_{\text{Rate of change in internal, kinetic, potential, etc. energies}} = 0$$

$$\dot{E}_{\text{in}} = \dot{E}_{\text{out}}$$

$$\dot{m} \left( h_1 + \frac{V_1^2}{2} \right) = \dot{m} \left( h_2 + \frac{V_2^2}{2} \right) + \dot{W}_{\text{out}}$$

$$\dot{W}_{\text{out}} = \dot{m} \left( h_1 - h_2 + \frac{V_1^2 - V_2^2}{2} \right) = \dot{m} \left( c_p (T_1 - T_2) + \frac{V_1^2 - V_2^2}{2} \right)$$

$$1 \text{ MPa}$$

$$500^{\circ}\text{C}$$

$$40 \text{ m/s}$$

$$100 \text{ kPa}$$

$$150^{\circ}\text{C}$$

The specific volume of air at the inlet and the mass flow rate are

$$\mathbf{v}_1 = \frac{RT_1}{P_1} = \frac{(0.287 \text{ kPa} \cdot \text{m}^3/\text{kg} \cdot \text{K})(500 + 273 \text{ K})}{1000 \text{ kPa}} = 0.2219 \text{ m}^3/\text{kg}$$

$$\dot{m} = \frac{A_1 V_1}{\mathbf{v}_1} = \frac{(0.2 \text{ m}^2)(40 \text{ m/s})}{0.2219 \text{ m}^3/\text{kg}} = \mathbf{36.06 \text{ kg/s}}$$

Similarly at the outlet,

$$\mathbf{v}_2 = \frac{RT_2}{P_2} = \frac{(0.287 \text{ kPa} \cdot \text{m}^3/\text{kg} \cdot \text{K})(150 + 273 \text{ K})}{100 \text{ kPa}} = 1.214 \text{ m}^3/\text{kg}$$

$$V_2 = \frac{\dot{m}\mathbf{v}_2}{A_2} = \frac{(36.06 \text{ kg/s})(1.214 \text{ m}^3/\text{kg})}{1 \text{ m}^2} = 43.78 \text{ m/s}$$

(b) Substituting into the energy balance equation gives

$$\begin{split} \dot{W}_{\text{out}} &= \dot{m} \Bigg( c_p (T_1 - T_2) + \frac{V_1^2 - V_2^2}{2} \Bigg) \\ &= (36.06 \, \text{kg/s}) \Bigg[ (1.051 \, \text{kJ/kg} \cdot \text{K}) (500 - 150) \text{K} + \frac{(40 \, \text{m/s})^2 - (43.78 \, \text{m/s})^2}{2} \Bigg( \frac{1 \, \text{kJ/kg}}{1000 \, \text{m}^2/\text{s}^2} \Bigg) \Bigg] \\ &= \textbf{13,260 \, kW} \end{split}$$