**15-80** Propane is burned with stoichiometric and 50 percent excess air. The adiabatic flame temperature is to be determined for both cases.

Assumptions 1 Steady operating conditions exist. 2 Air and combustion gases are ideal gases. 3 Kinetic and potential energies are negligible. 4 There are no work interactions. 5 The combustion chamber is adiabatic.

Analysis Under steady-flow conditions the energy balance  $E_{\rm in} - E_{\rm out} = \Delta E_{\rm system}$  applied on the combustion chamber with Q = W = 0 reduces to

$$\sum N_P \left( \overline{h}_f^{\,\circ} + \overline{h} - \overline{h}^{\,\circ} \right)_P = \sum N_R \left( \overline{h}_f^{\,\circ} + \overline{h} - \overline{h}^{\,\circ} \right)_R \longrightarrow \sum N_P \left( \overline{h}_f^{\,\circ} + \overline{h} - \overline{h}^{\,\circ} \right)_P = \sum N_R \overline{h}_{f,R}^{\,\circ}$$

since all the reactants are at the standard reference temperature of 25°C. Then, for the stoicihiometric air

$$C_3H_8 + a_{th}(O_2 + 3.76 N_2) \longrightarrow 3 CO_2 + 4 H_2O + a_{th} \times 3.76 N_2$$

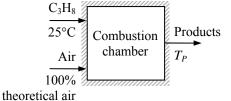
where  $a_{th}$  is the stoichiometric coefficient and is determined from the  $O_2$  balance,

$$a_{th} = 3 + 2 = 5$$

Thus,

$$C_3H_8 + 5(O_2 + 3.76 N_2) \longrightarrow 3CO_2 + 4H_2O + 18.8 N_2$$

From the tables,



	$\overline{\mathbf{h}}_{\mathbf{f}}^{\circ}$	$\overline{\mathbf{h}}_{\mathbf{298K}}$
Substance	kJ/kmol	kJ/kmol
$C_3H_8(g)$	-103,850	
$\mathrm{O}_2$	0	8682
$N_2$	0	8669
$H_2O(g)$	-241,820	9904
$CO_2$	-393,520	9364

Thus,

$$(3)\left(-393,520 + \overline{h}_{CO2} - 9364\right) + (4)\left(-241,820 + \overline{h}_{H2O} - 9904\right) + (18.8)\left(0 + \overline{h}_{N2} - 8669\right) = (1)\left(-103,850\right) + 0 + 0$$

It yields  $3\bar{h}_{CO2} + 4\bar{h}_{H2O} + 18.8\bar{h}_{N2} = 2,274,680 \text{ kJ}$ 

The adiabatic flame temperature is obtained from a trial and error solution. A first guess is obtained by dividing the right-hand side of the equation by the total number of moles, which yields 2,274,680/(3+4+18.8)=88,166 kJ/kmol. This enthalpy value corresponds to about 2650 K for N<sub>2</sub>. Noting that the majority of the moles are N<sub>2</sub>,  $T_P$  will be close to 2650 K, but somewhat under it because of the higher specific heat of H<sub>2</sub>O.

At 2500 K:

$$3\overline{h}_{CO2} + 4\overline{h}_{H2O} + 18.8\overline{h}_{N2} = 3 \times 131,290 + 4 \times 108,868 + 18.8 \times 82,981$$
  
= 2,389,380 kJ (Higher than 2,274,680 kJ)

At 2450 K:

$$3\overline{h}_{CO2} + 4\overline{h}_{H2O} + 18.8\overline{h}_{N2} = 3 \times 128,219 + 4 \times 106,183 + 18.8 \times 81,149$$
  
= 2,334,990 kJ (Higher than 2,274,680 kJ)

At 2400 K:

$$3\overline{h}_{CO2} + 4\overline{h}_{H2O} + 18.8\overline{h}_{N2} = 3 \times 125,152 + 4 \times 103,508 + 18.8 \times 79,320$$
  
= 2,280,704 kJ (Higher than 2,274,680 kJ)

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At 2350 K:

$$3\overline{h}_{CO2} + 4\overline{h}_{H2O} + 18.8\overline{h}_{N2} = 3 \times 122,091 + 4 \times 100,846 + 18.8 \times 77,496$$
  
= 2,226,580 kJ (Lower than 2,274,680 kJ)

By interpolation of the two results,

$$T_P = 2394 \text{ K} = 2121^{\circ}\text{C}$$

When propane is burned with 50% excess air, the reaction equation may be written as

$$C_3H_8 + 1.5 \times a_{th}(O_2 + 3.76N_2) \longrightarrow 3CO_2 + 4H_2O + 0.5 \times a_{th}O_2 + 1.5 \times a_{th} \times 3.76N_2$$

where  $a_{th}$  is the stoichiometric coefficient and is determined from the  $O_2$  balance,

$$1.5a_{th} = 3 + 2 + 0.5a_{th} \longrightarrow a_{th} = 5$$
Thus,
$$C_{3}H_{8} + 7.5(O_{2} + 3.76N_{2}) \longrightarrow 3CO_{2} + 4H_{2}O + 2.5O_{2} + 28.2N_{2}$$

$$C_{3}H_{8} + 7.5(O_{2} + 3.76N_{2}) \longrightarrow 3CO_{2} + 4H_{2}O + 2.5O_{2} + 28.2N_{2}$$

$$C_{3}H_{8} + 7.5(O_{2} + 3.76N_{2}) \longrightarrow 3CO_{2} + 4H_{2}O + 2.5O_{2} + 28.2N_{2}$$

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$$C_{3}H_{8} + 7.5(O_{2} + 3.76N_{2}) \longrightarrow 3CO_{2} + 4H_{2}O + 2.5O_{2} + 28.2N_{2}$$

Using the values in the table.

$$(3) \left(-393,520 + \overline{h}_{\text{CO2}} - 9364\right) + (4) \left(-241,820 + \overline{h}_{\text{H2O}} - 9904\right) + (2.5) \left(0 + \overline{h}_{\text{O2}} - 8682\right) + (28.2) \left(0 + \overline{h}_{\text{N2}} - 8669\right) = (1) \left(-103,850\right) + 0 + 0$$

It yields 
$$3\overline{h}_{CO2} + 4\overline{h}_{H2O} + 2.5\overline{h}_{O2} + 28.2\overline{h}_{N2} = 2,377,870 \text{ kJ}$$

The adiabatic flame temperature is obtained from a trial and error solution. A first guess is obtained by dividing the right-hand side of the equation by the total number of moles, which yields 2,377,870/(3+4+2.5+28.2) = 63,073 kJ/kmol. This enthalpy value corresponds to about 1960 K for N<sub>2</sub>. Noting that the majority of the moles are N<sub>2</sub>,  $T_P$  will be close to 1960 K, but somewhat under it because of the higher specific heat of H<sub>2</sub>O.

At 1800 K:

$$3\overline{h}_{CO2} + 4\overline{h}_{H2O} + 2.5\overline{h}_{O2} + 28.2\overline{h}_{N2} = 3 \times 88,806 + 4 \times 72,513 + 2.5 \times 60,371 + 28.2 \times 57,651$$
  
= 2.333,160 kJ (Lower than 2.377,870 kJ)

At 1840 K:

$$3\overline{h}_{CO2} + 4\overline{h}_{H2O} + 2.5\overline{h}_{O2} + 28.2\overline{h}_{N2} = 3 \times 91,196 + 4 \times 74,506 + 2.5 \times 61,866 + 28.2 \times 59,075$$
  
= 2,392,190 kJ (Higher than 2,377,870 kJ)

By interpolation,

$$T_P = 1830 \text{ K} = 1557^{\circ}\text{C}$$