

# *Review of First and Second Law of Thermodynamics*



## **Reading**

2-6, 4-1, 4-2

5-1 → 5-3

6-1, 6-2, 7-13

## **Problems**

4-27, 4-40, 4-41

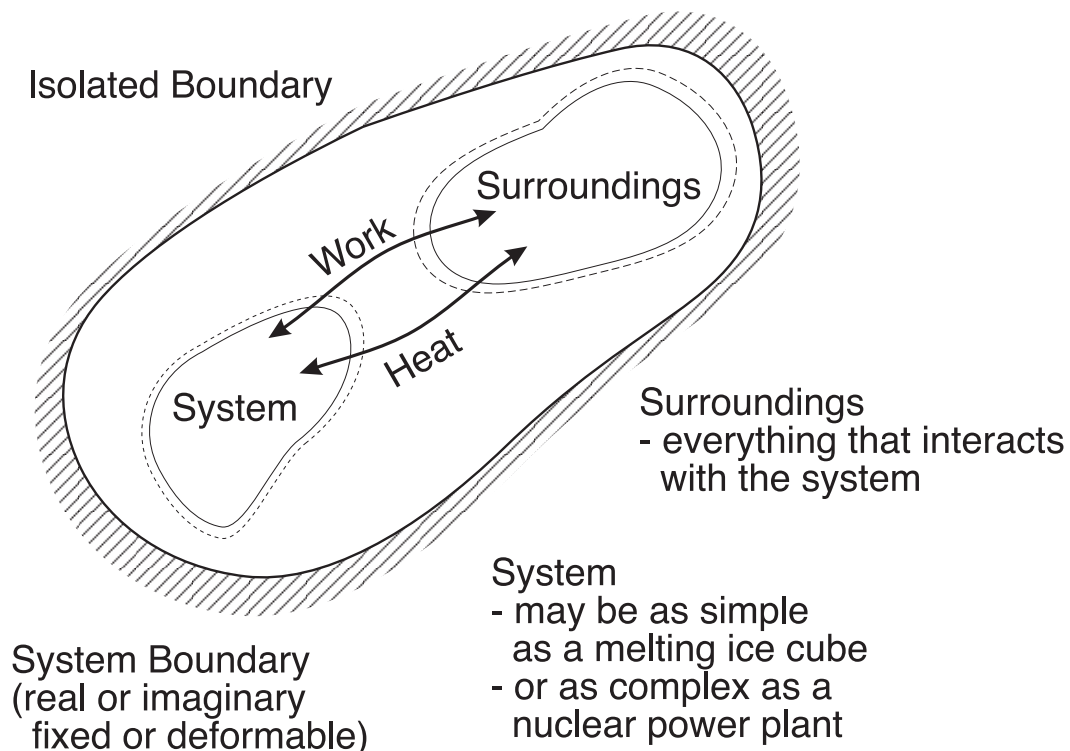
## **Definitions**

### **SYSTEM:**

- any specified collection of matter under study.
- all systems possess properties like mass, energy, entropy, volume, pressure, temperature, etc.

### **WORK & HEAT TRANSFER:**

- thermodynamics deals with these properties of matter as a system interacts with its surroundings through work and heat transfer
- work and heat transfer are NOT properties → they are the forms that energy takes to cross the system boundary



# First Law of Thermodynamics

## Control Mass (Closed System)

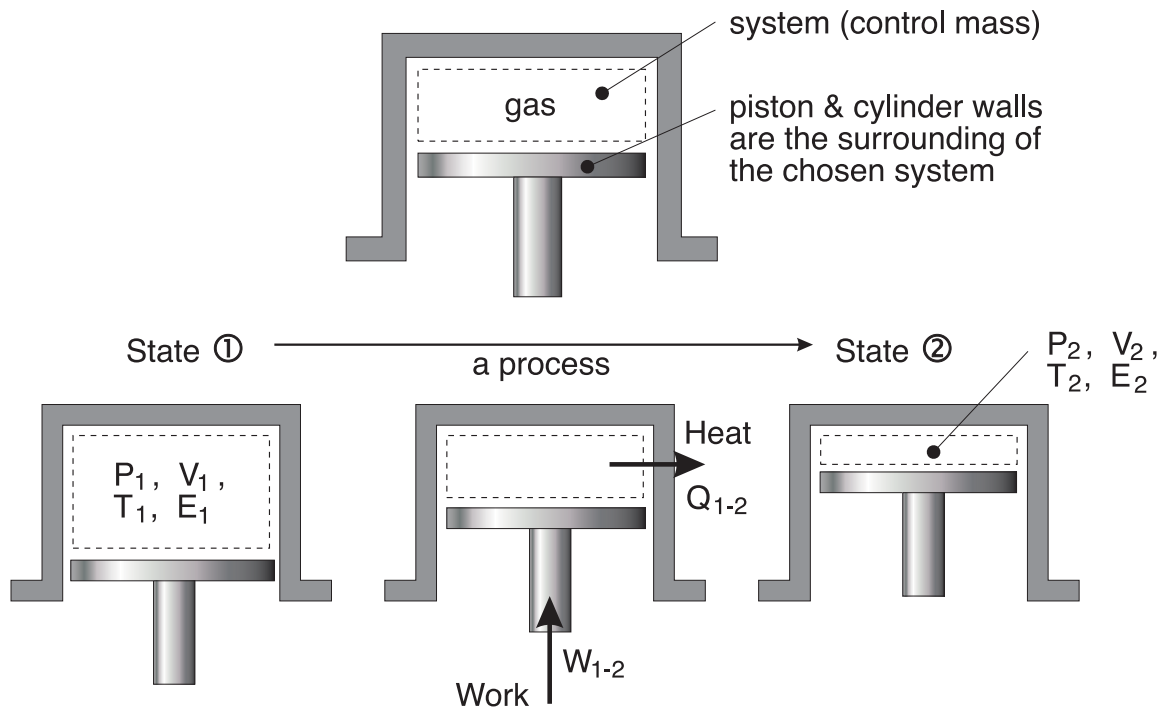
### CONSERVATION OF ENERGY:

- the energy content of an isolated system is constant

$$\text{energy entering} - \text{energy leaving} = \text{change of energy within the system}$$

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### Example: A Gas Compressor



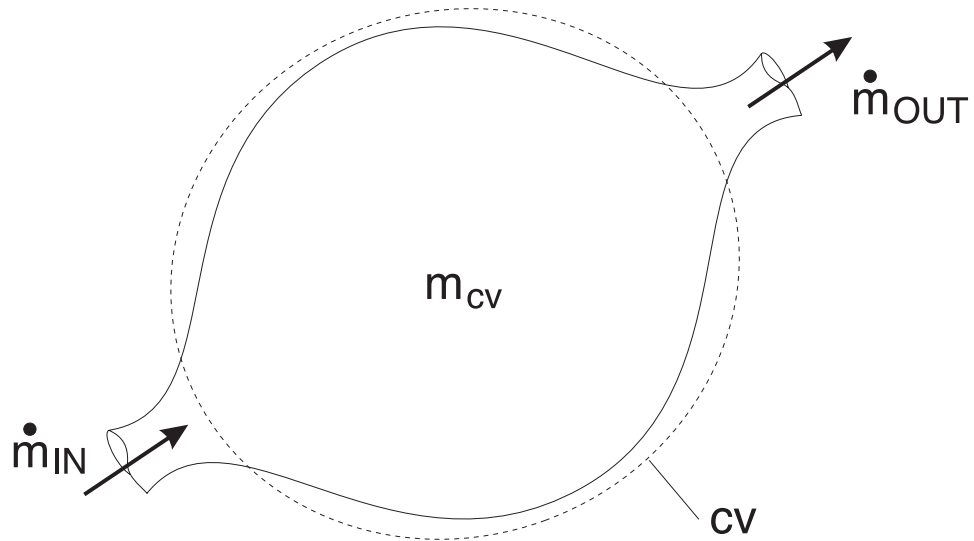
Performing a 1st law energy balance:

$$\left\{ \begin{array}{l} \text{Initial} \\ \text{Energy} \\ E_1 \end{array} \right\} + \left\{ \begin{array}{l} \text{Energy gain } W_{1-2} \\ \text{Energy loss } Q_{1-2} \end{array} \right\} = \left\{ \begin{array}{l} \text{Final} \\ \text{Energy} \\ E_2 \end{array} \right\}$$

$$\boxed{E_1 + W_{1-2} - Q_{1-2} = E_2}$$

## Control Volume Analysis (Open System)

### CONSERVATION OF MASS:



$$\left\{ \begin{array}{l} \text{rate of increase} \\ \text{of mass within} \\ \text{the CV} \end{array} \right\} = \left\{ \begin{array}{l} \text{net rate of} \\ \text{mass flow} \\ IN \end{array} \right\} - \left\{ \begin{array}{l} \text{net rate of} \\ \text{mass flow} \\ OUT \end{array} \right\}$$

$$\frac{d}{dt}(m_{CV}) = \dot{m}_{IN} - \dot{m}_{OUT}$$

where:

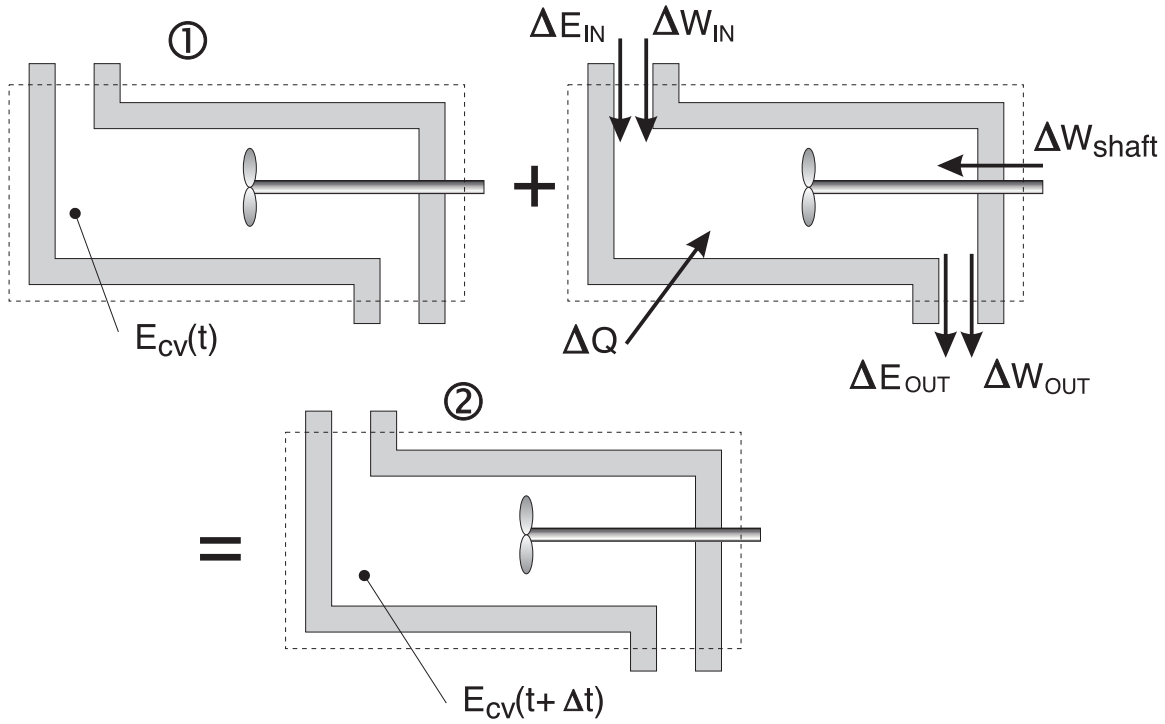
$$m_{CV} = \int_V \rho dV$$

$$\dot{m}_{IN} = (\rho v^* A)_{IN}$$

$$\dot{m}_{OUT} = (\rho v^* A)_{OUT}$$

with  $v^* =$  average velocity

**CONSERVATION OF ENERGY:**



The 1st law states:

$$E_{CV}(t) + \Delta Q + \Delta W_{shaft} + (\Delta E_{IN} - \Delta E_{OUT}) + (\Delta W_{IN} - \Delta W_{OUT}) = E_{CV}(t + \Delta t) \quad (1)$$

where:

$$\Delta E_{IN} = e_{IN} \Delta m_{IN}$$

$$\Delta E_{OUT} = e_{OUT} \Delta m_{OUT}$$

$$\Delta W = \text{flow work}$$

$$e = \frac{E}{m} = \underbrace{u}_{\text{internal}} + \underbrace{\frac{(v^*)^2}{2}}_{\text{kinetic}} + \underbrace{gz}_{\text{potential}}$$

# Second Law of Thermodynamics

## Fundamentals

1. Like mass and energy, every system has entropy.

*Entropy is a measure of the degree of microscopic disorder and represents our uncertainty about the microscopic state.*

2. Unlike mass and energy, entropy can be produced but it can never be destroyed. That is, the entropy of a system plus its surroundings (i.e. an isolated system) can never decrease (2nd law).

$$\mathcal{P}_m = m_2 - m_1 = 0 \text{ (conservation of mass)}$$

$$\mathcal{P}_E = E_2 - E_1 = 0 \text{ (conservation of energy)} \rightarrow \text{1st law}$$

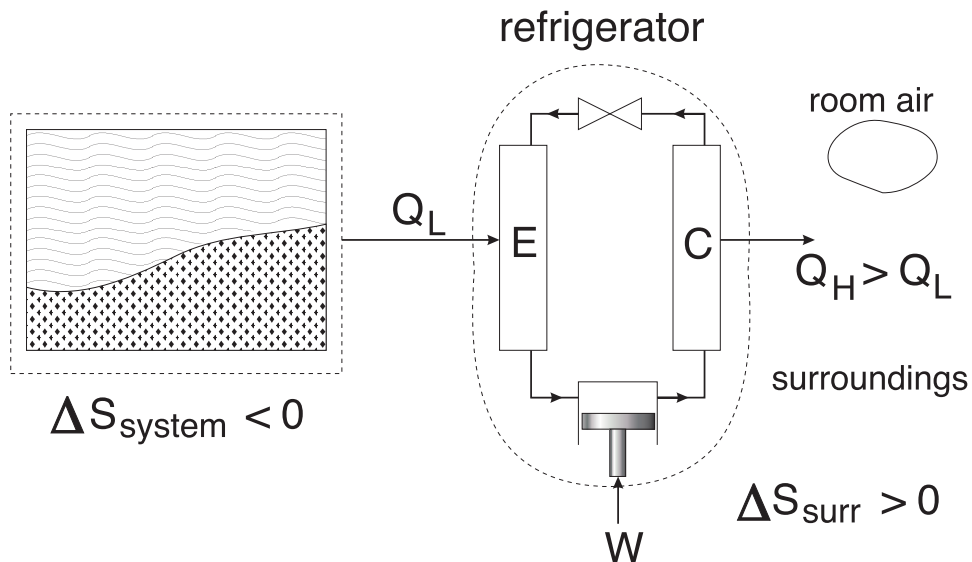
$$\mathcal{P}_S = S_2 - S_1 \geq 0 \rightarrow \text{2nd law}$$

The second law states:

$$(\Delta S)_{system} + (\Delta S)_{surr.} \geq 0$$

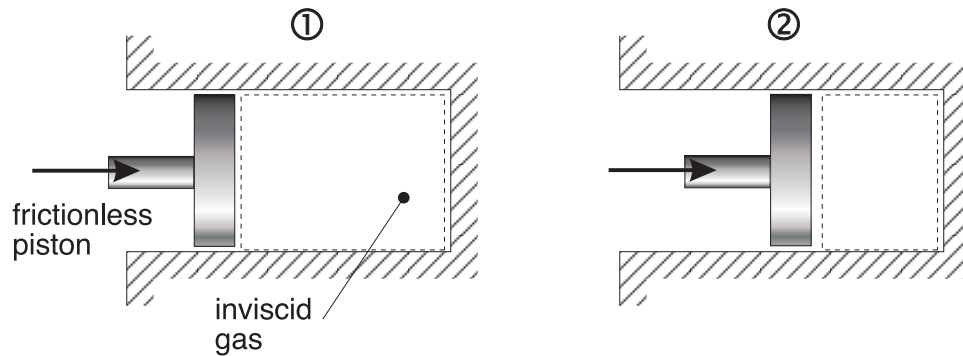
where  $\Delta \equiv final - initial$

### Example: A freezing process



3. **Reference:** In a perfect crystal of a pure substance at  $T = 0\text{ K}$ , the molecules are completely motionless and are stacked precisely in accordance with the crystal structure. Since entropy is a measure of microscopic disorder, then in this case  $S = 0$ . That is, there is no uncertainty about the microscopic state.
4. **Relationship to Work:** For a given system, an increase in the microscopic disorder (that is an increase in entropy) results in a loss of ability to do useful work.
5. **Heat:** Energy transfer as heat takes place as work at the microscopic level but in a random, disorganized way. This type of energy transfer carries with it some chaos and thus results in entropy flow in or out of the system.
6. **Work:** Energy transfer by work is microscopically organized and therefore entropy-free.

**Example: Slow adiabatic compression of a gas**



Idealization - which makes the process completely reversible

A process  $1 \rightarrow 2$  is said to be reversible if the reverse process  $2 \rightarrow 1$  restores the system to its original state without leaving any change in either the system or its surroundings.

$\rightarrow$  idealization where  $S_2 = S_1 \Rightarrow \mathcal{P}_S = 0$

$T_2 > T_1 \Rightarrow$  increased microscopic disorder

$V_2 < V_1 \Rightarrow$  reduced uncertainty about the whereabouts of molecules

$$\underbrace{\text{Reversible}}_{\mathcal{P}_S=0} + \underbrace{\text{Adiabatic Process}}_{Q=0} \Rightarrow \underbrace{\text{Isentropic Process}}_{S_1=S_2}$$

The 2nd law states:

$$\mathcal{P}_S = (\Delta S)_{\text{system}} + (\Delta S)_{\text{surr}} \geq 0$$

where:

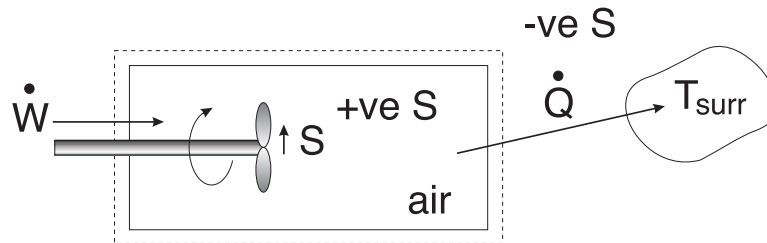
$> 0$  irreversible (real world)

$= 0$  reversible (frictionless, perfectly elastic, inviscid fluid)

But does:

*Isentropic Process  $\Rightarrow$  Reversible + Adiabatic*

NOT ALWAYS - the entropy increase of a substance during a process as a result of irreversibilities may be offset by a decrease in entropy as a result of heat losses.



## General Derivation of Gibb's Equation

From a 1st law energy balance when KE and PE are neglected

*Energy Input = Energy Output + Increase in Energy Storage*

$$\underbrace{dQ}_{\text{amount}} = dW + \underbrace{dU}_{\text{differential}} \quad (1)$$

We know that the differential form of entropy is

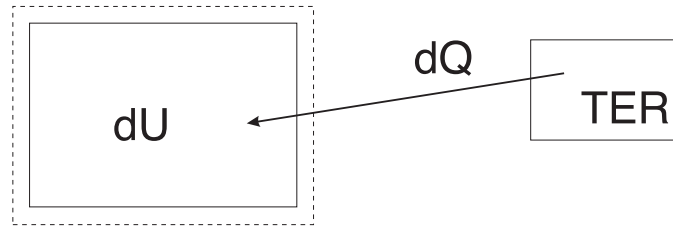
$$dS = \frac{dQ}{T} \quad (2)$$

$$dW = PdV \quad (3)$$

Combining Eqs. 1, 2 and 3

$$dS = \frac{dU}{T} + \frac{PdV}{T} \Rightarrow \underbrace{ds = \frac{du}{T} + \frac{Pdv}{T}}_{\text{per unit mass}}$$

## Second Law Analysis for a Control Mass



- control mass is uniformly at  $T_{TER}$  at all times
- control mass has a fixed size ( $V = \text{constant}$ )

From Gibb's equation

$$T_{TER} dS = dU + P dV^0$$

From the 1st law

$$dU = dQ$$

Therefore for a reversible process

$$dS = \frac{dQ}{T_{TER}}$$

We integrate to give

$$S_2 - S_1 = \frac{Q_{1-2}}{T_{TER}}$$

and for a non-reversible process

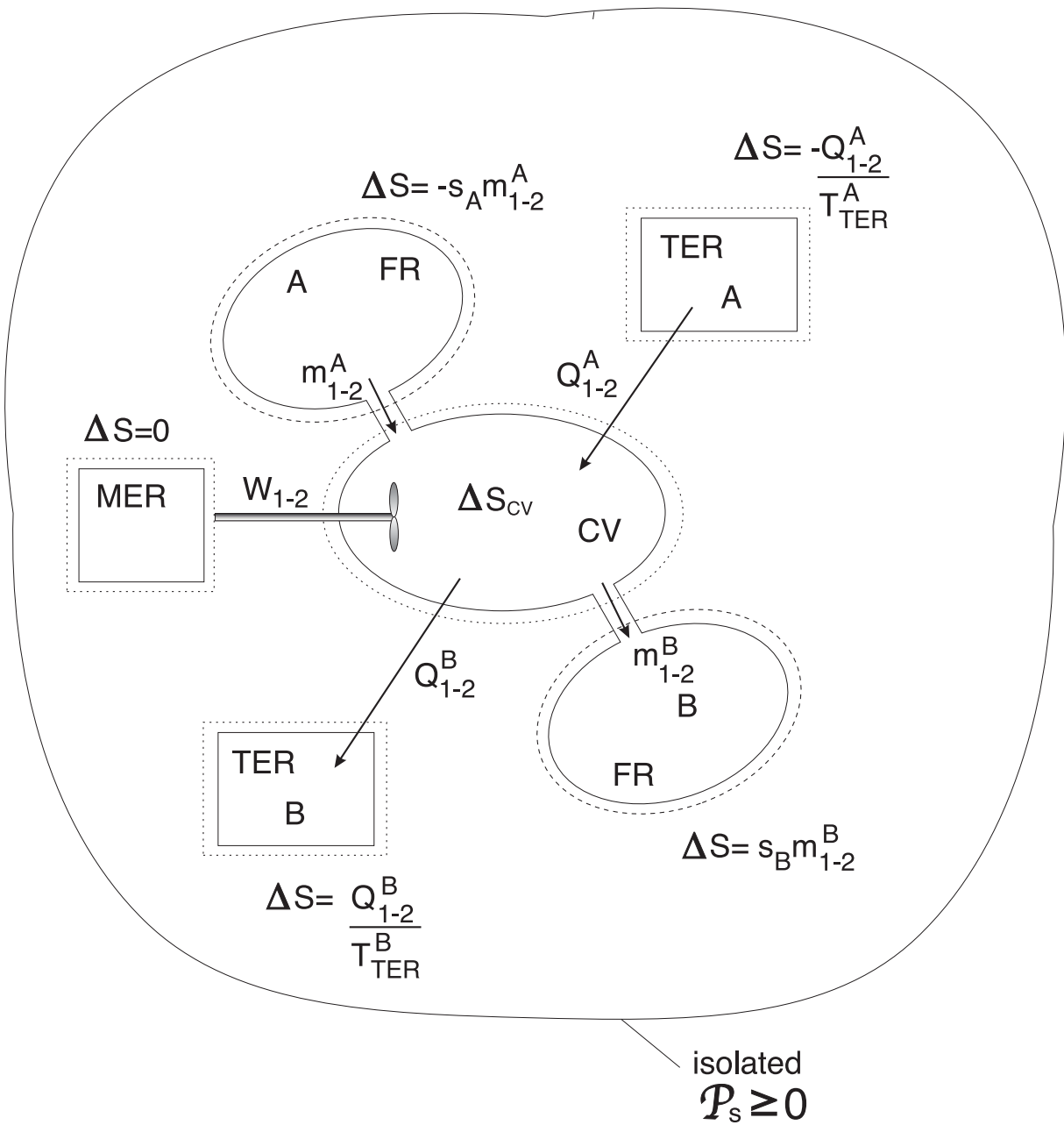
$$dS = \frac{dQ}{T_{TER}} + d\mathcal{P}_S$$

We integrate to give

$$S_2 - S_1 = \frac{Q_{1-2}}{T_{TER}} + \mathcal{P}_{S_{1-2}}$$



## Second Law Analysis for a Control Volume



where:

- FR - fluid reservoir
- TER - thermal energy reservoir
- MER - mechanical energy reservoir

For the isolated system

$$(\Delta S)_{sys} + (\Delta S)_{sur} = \mathcal{P}_{S_{1-2}} \geq 0$$

$$\Delta S_{CV} - s_A m_{1-2}^A + s_B m_{1-2}^B - \frac{Q_{1-2}^A}{T_{TER}^A} + \frac{Q_{1-2}^B}{T_{TER}^B} = \mathcal{P}_{S_{1-2}}$$

or as a rate equation

$$\left( \frac{dS}{dt} \right)_{CV} = \left( s\dot{m} + \frac{\dot{Q}}{T_{TER}} \right)_{IN} - \left( s\dot{m} + \frac{\dot{Q}}{T_{TER}} \right)_{OUT} + \dot{\mathcal{P}}_S$$

This can be thought of as

$$accumulation = IN - OUT + generation$$