Rankine Cycle



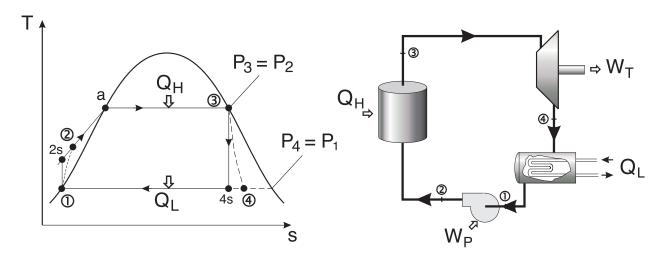
Reading $10-2 \rightarrow 10-7$

Problems

10-16, 10-34, 10-37, 10-44, 10-47, 10-59

Definitions

- working fluid is alternately vaporized and condensed as it recirculates in a closed cycle
- water is typically used as the working fluid because of its low cost and relatively large value of enthalpy of vaporization
- the standard vapour cycle that excludes internal irreversibilities is called the **Ideal Rankine**Cycle



- ullet the condensation process is allowed to proceed to completion between state points $4 \to 1$
 - provides a saturated liquid at 1
- the water at state point 1 can be conveniently pumped to the boiler pressure at state point 2
- but the water is <u>not</u> at the saturation temperature corresponding to the boiler pressure
- heat must be added to change the water at 2 to saturated water at 'a'
- ullet when heat is added at non-constant temperature (between 2-a), the cycle efficiency will decrease

Analyze the Process

Assume steady flow, KE = PE = 0.

From a 1st law balance, we know

$$energy in = energy out$$

Device	1st Law Balance			
Boiler	$h_2+q_H=h_3$	\Rightarrow	$q_H=h_3-h_2$	(in)
Turbine	$h_3=h_4+w_T$	\Rightarrow	$w_T = h_3 - h_4$	(out)
Condenser	$h_4=h_1+q_L$	\Rightarrow	$q_L=h_4-h_1$	(out)
Pump	$h_1+w_P=h_2$	\Rightarrow	$w_P = h_2 - h_1$	(in)

The net work output is given as

$$w_T - w_p = (h_3 - h_4) - (h_2 - h_1)$$

= $(h_3 - h_4) + (h_1 - h_2)$

The net heat supplied to the boiler is

$$q_H = (h_3 - h_2)$$

The Rankine efficiency is

$$egin{array}{ll} \eta_R &=& rac{net \, work \, output}{heat \, supplied \, to \, the \, boiler} \ &=& rac{(h_3-h_4)+(h_1-h_2)}{(h_3-h_2)} \end{array}$$

If we consider the fluid to be incompressible

$$(h_2 - h_1) = v(P_2 - P_1)$$

Since the actual process is irreversible, an isentropic efficiency can be defined such that

Expansion process \Rightarrow Isentropic efficiency = $\frac{\text{actual work}}{\text{isentropic work}}$

Compression process \Rightarrow Isentropic efficiency = $\frac{\text{isentropic work}}{\text{actual work}}$

Both isentropic efficiencies will have a numerical value between 0 and 1.

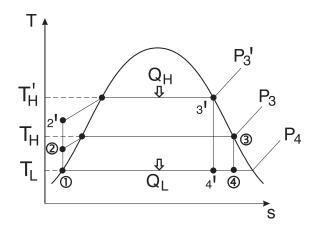
Effects of Boiler and Condenser Pressure

We know the efficiency is proportional to

$$\eta \propto 1 - rac{T_L}{T_H}$$

The question is \rightarrow how do we increase efficiency \Rightarrow $T_L \downarrow$ and/or $T_H \uparrow$.

1. INCREASED BOILER PRESSURE:



- ullet an increase in boiler pressure results in a higher T_H for the same T_L , therefore $\eta\uparrow$.
- but 4' has a lower quality than 4
 - wetter steam at the turbine exhaust

- results in cavitation of the turbine blades
- η ↓ plus ↑ maintenance
- quality should be > 80% at the turbine exhaust

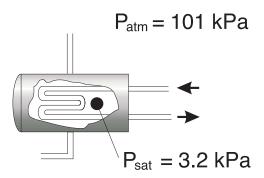
2. LOWER T_L :

 \bullet we are generally limited by the TER (lake, river, etc.)

eg. lake @
$$15~^{\circ}C+\underbrace{\Delta T=10~^{\circ}C}_{resistance~to~HT}=25~^{\circ}C$$

$$\Rightarrow P_{sat} = 3.2 \, kPa.$$

- this is why we have a condenser
 - the pressure at the exit of the turbine can be less than atmospheric pressure
 - the closed loop of the condenser allows us to use treated water on the cycle side
 - but if the pressure is less that atmospheric pressure, air can leak into the condenser, preventing condensation



3. INCREASED T_H BY ADDING SUPERHEAT:

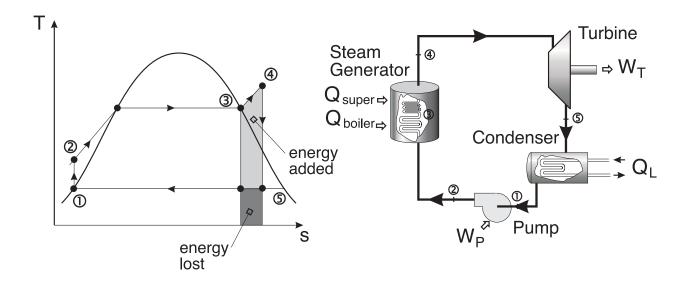
- the average temperature at which heat is supplied in the boiler can be increased by superheating the steam
 - dry saturated steam from the boiler is passed through a second bank of smaller bore tubes within the boiler until the steam reaches the required temperature

The advantage is

$$\eta = rac{W_{net} \uparrow}{Q_H \uparrow} \;\; overall \uparrow$$

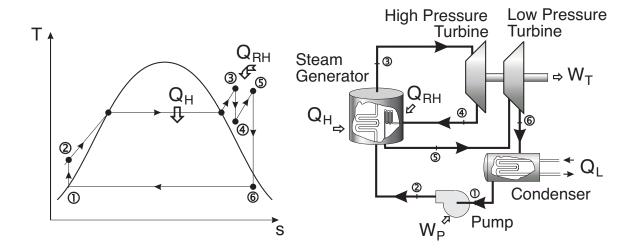
The value of \overline{T}_H , the mean temperature at which heat is added, increases, while \overline{T}_L remains constant. Therefore the efficiency increases.

- the quality of the turbine exhaust increases, hopefully where x>0.9
- with sufficient superheating the turbine exhaust can fall in the superheated region.



Rankine Cycle with Reheat

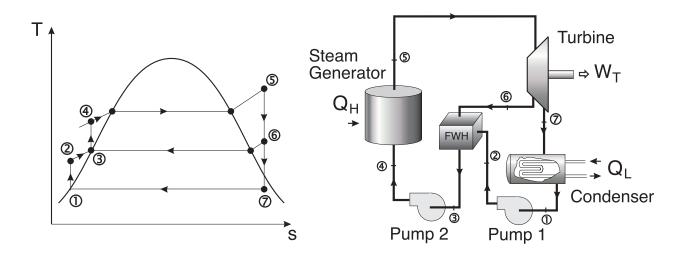
- the wetness at the exhaust of the turbine should be no greater that 10% this can result in physical erosion of the turbine blades
- but high boiler pressures are required for high efficiency tends to lead to a high wetness ratio
- to improve the exhaust steam conditions, the steam can be reheated with the expansion carried out in two steps



- the temperature of the steam entering the turbine is limited by metallurgical constraints
- ullet modern boilers can handle up to 30~MPa and a maximum temperature of $T_{max}pprox 650~^{\circ}C$.
- ullet newer materials, such as ceramic blades can handle temperatures up to $750\,{}^{\circ}C$.

Rankine Cycle with Regeneration

- ullet Carnot cycle has efficiency: $\eta=1-T_L/T_H$
 - add Q_H at as high a T_H as possible
 - reject Q_L at as low a T_L as possible
- the Rankine cycle can be used with a *Feedwater Heater* to heat the high pressure sub-cooled water at the pump exit to the saturation temperature
 - most of the heat addition $\left(Q_{H}
 ight)$ is done at high temperature



Feedwater Heaters

There are two different types of feedwater heaters

- 1. *OPEN FWH*: the streams mix \rightarrow high temperature steam with low temperature water at constant pressure
- 2. *CLOSED FWH*: a heat exchanger is used to transfer heat between the two streams but the streams do *not* mix. The two streams can be maintained at different pressures.

1. *OPEN FWH*:

- working fluid passes isentropically through the turbine stages and pumps
- steam enters the first stage turbine at state 1 and expands to state 2 where a fraction of the total flow is bled off into an open feedwater heater at P_2
- the rest of the steam expands into the second stage turbine at state point 3 this portion of the fluid is condensed and pumped as a saturated liquid to the FWH at P_2
- a single mixed stream exists the FWH at state point 6

Analysis:

• we must determine the mass flow rates through each of the components. By performing an <u>mass balance</u> over the turbine

$$\dot{m}_6 + \dot{m}_7 = \dot{m}_5 \tag{1}$$

If we normalize Eq. (1) with respect the total mass flow rate \dot{m}_1

$$\frac{\dot{m}_6}{\dot{m}_5} + \frac{\dot{m}_7}{\dot{m}_5} = 1 \tag{2}$$

Let the flow at state point 2 be

$$y=rac{\dot{m}_6}{\dot{m}_5}$$

Therefore

$$\frac{\dot{m}_7}{\dot{m}_5} = 1 - y \tag{3}$$

Assuming no heat loss at the FWH, establish an energy balance across the FWH

$$yh_6 + (1-y)h_2 = 1 \cdot h_3$$

$$y = rac{h_3 - h_2}{h_6 - h_2} = rac{\dot{m}_6}{\dot{m}_5}$$

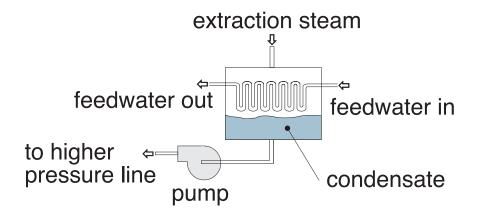
and

$$1-y=rac{\dot{m}_7}{\dot{m}_5}$$

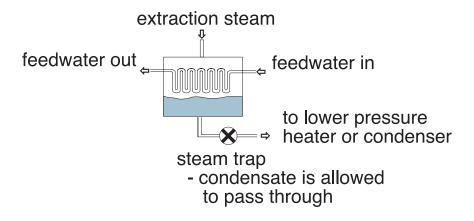
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2. CLOSED FWH:

- two variations exist
 - (a) pump the condensate back to the high pressure line



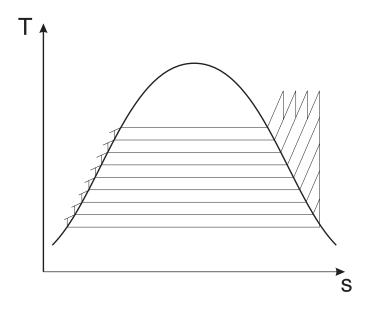
- a steam trap is inserted in the condensed steam line that allows only liquid to pass
 - liquid is passed to a low pressure region such as the condenser or a low pressure heater



- the incoming feedwater does not mix with the extracted steam
 - both streams flow separately through the heater
 - the two streams can have different pressures

Other Topics

"IDEAL" RANKINE CYCLE:



- too expensive to build
- requires multiple reheat and regeneration cycles
- approaches Carnot efficiency

TOPPING CYCLE (BINARY CYCLE):

- involves two Rankine cycles running in tandem with different working fluids such as mercury and water
- why:
 - typically a boiler will supply energy at $1300-1400\,^{\circ}C$
 - but $T_{critical}$ for water is $374.14~^{\circ}C$
 - * most energy is absorbed below this temperature
 - * high ΔT between the boiler source and the water leads to a major source of irreversibilities
 - $T_{critical}$ for mercury is about $1500~^{\circ}C$
 - * no need for superheating
 - combine the large enthalpy of evaporation of water at low temperatures with the advantages of mercury at high temperatures
 - in addition, the mercury dome leads to a high quality at the exit of the turbine