

Review of First and Second Law of Thermodynamics



Reading

4-1 \rightarrow 4-4

5-2 \rightarrow 5-4, 5.7

6-1 \rightarrow 6-13, 6-13

Problems

4-32, 4-36, 4-87, 4-246

6-122, 6-127, 6-130

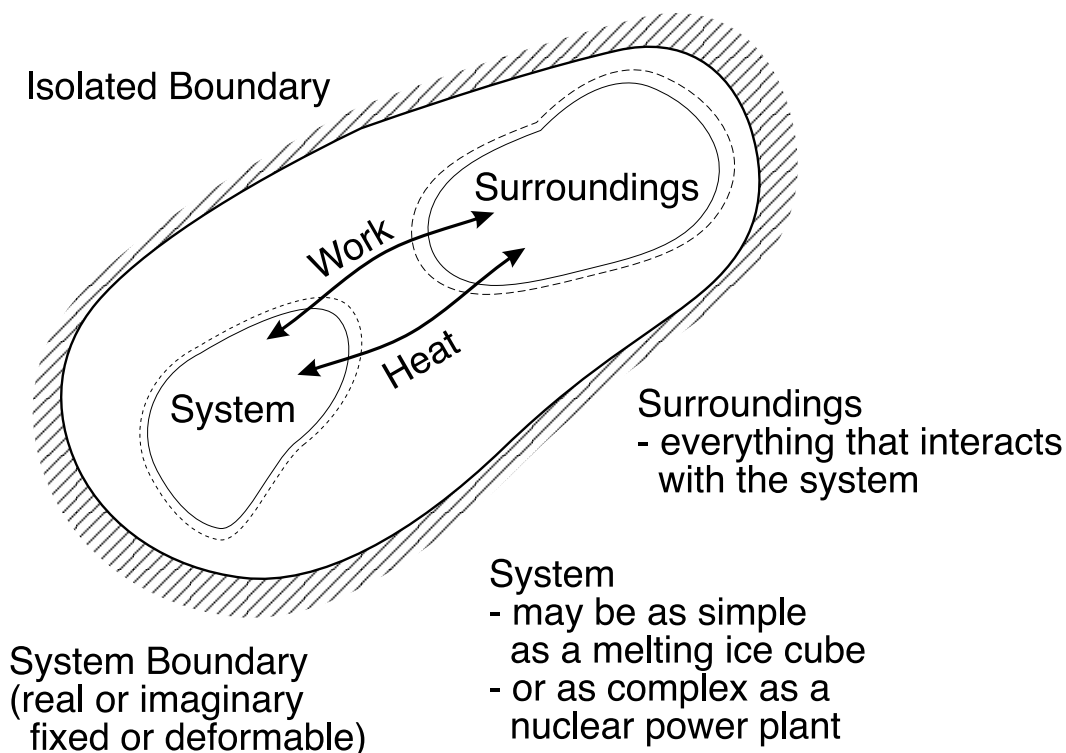
Definitions

SYSTEM:

- any specified collection of matter under study.
- all systems possess properties like mass, energy, entropy, volume, pressure, temperature, etc.

WORK & HEAT TRANSFER:

- thermodynamics deals with these properties of matter as a system interacts with its surroundings through work and heat transfer
- work and heat transfer are NOT properties \rightarrow they are the forms that energy takes to cross the system boundary



First Law of Thermodynamics

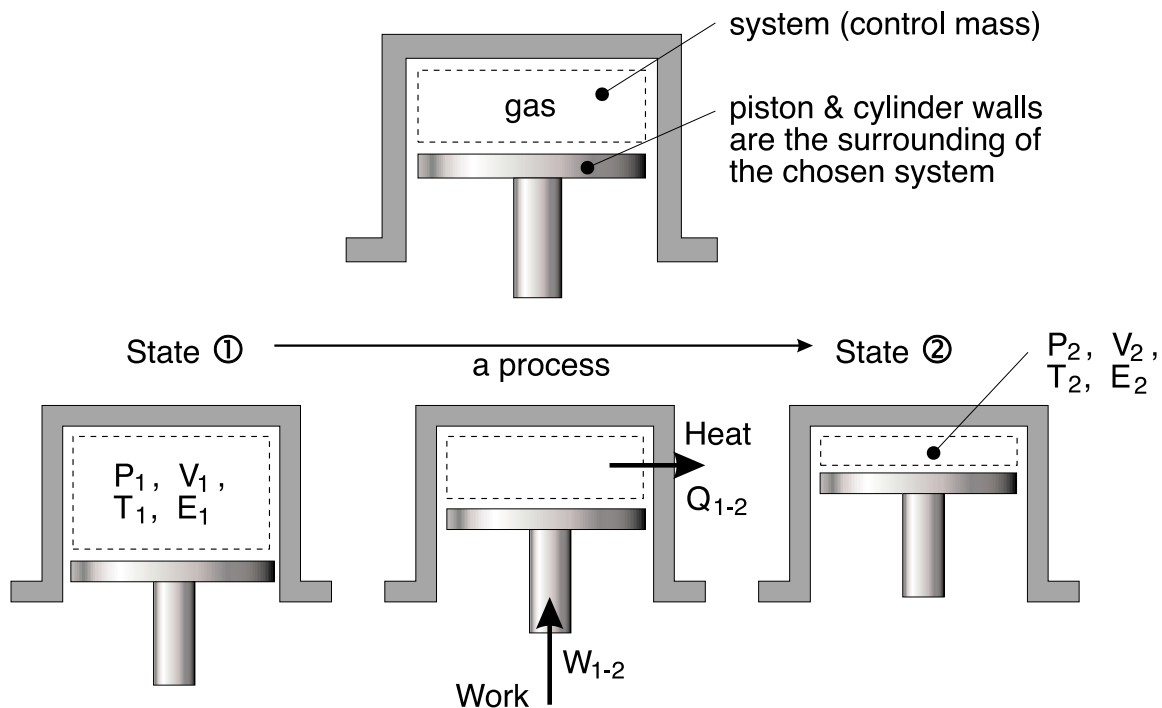
Control Mass (Closed System)

CONSERVATION OF ENERGY:

- the energy content of an isolated system is constant

energy entering – energy leaving = change of energy within the system

Example: A Gas Compressor



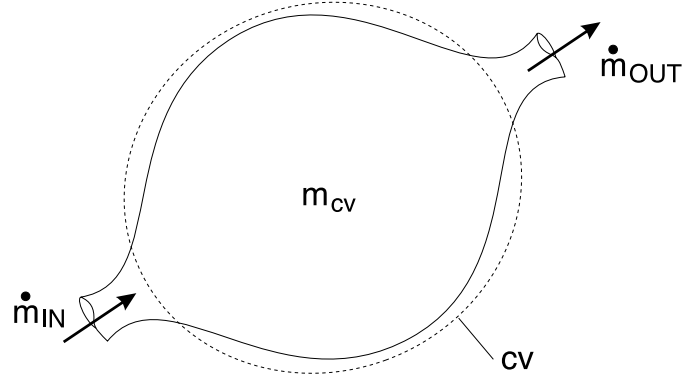
Performing a 1st law energy balance:

$$\left\{ \begin{array}{c} \textit{Initial} \\ \textit{Energy} \\ E_1 \end{array} \right\} + \left\{ \begin{array}{c} \textit{Energy gain } W_{1-2} \\ \textit{Energy loss } Q_{1-2} \end{array} \right\} = \left\{ \begin{array}{c} \textit{Final} \\ \textit{Energy} \\ E_2 \end{array} \right\}$$

$$\boxed{E_1 + W_{1-2} - Q_{1-2} = E_2}$$

Control Volume Analysis (Open System)

CONSERVATION OF MASS:



$$\left\{ \begin{array}{l} \text{rate of increase} \\ \text{of mass within} \\ \text{the CV} \end{array} \right\} = \left\{ \begin{array}{l} \text{net rate of} \\ \text{mass flow} \\ \text{IN} \end{array} \right\} - \left\{ \begin{array}{l} \text{net rate of} \\ \text{mass flow} \\ \text{OUT} \end{array} \right\}$$

$$\frac{d}{dt}(m_{CV}) = \dot{m}_{IN} - \dot{m}_{OUT}$$

where:

$$m_{CV} = \int_V \rho \, dV$$

$$\dot{m}_{IN} = (\rho \, v^* \, A)_{IN}$$

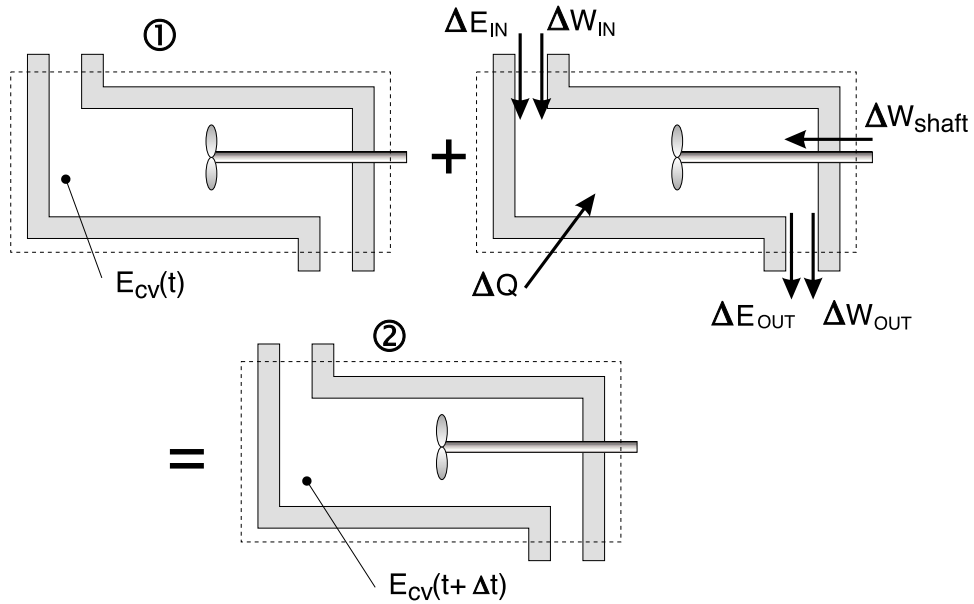
$$\dot{m}_{OUT} = (\rho \, v^* \, A)_{OUT}$$

with v^* = average velocity

CONSERVATION OF ENERGY:

The 1st law states:

$$\begin{aligned} E_{CV}(t) + \Delta Q + \Delta W_{shaft} + (\Delta E_{IN} - \Delta E_{OUT}) + \\ (\Delta W_{IN} - \Delta W_{OUT}) = E_{CV}(t + \Delta t) \end{aligned} \quad (1)$$



where:

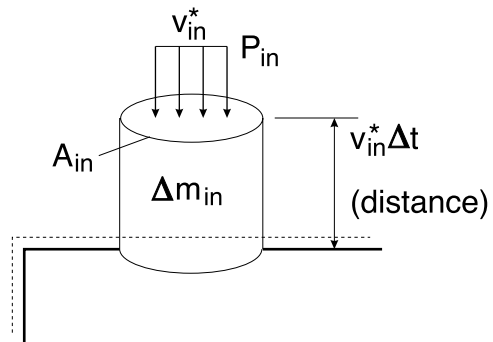
$$\Delta E_{IN} = e_{IN} \Delta m_{IN}$$

$$\Delta E_{OUT} = e_{OUT} \Delta m_{OUT}$$

$$\Delta W = \text{flow work}$$

$$e = \frac{E}{m} = \underbrace{u}_{\text{internal}} + \underbrace{\frac{(v^*)^2}{2}}_{\text{kinetic}} + \underbrace{gz}_{\text{potential}}$$

What is flow work?



$$\Delta m_{IN} = \rho_{IN} \overbrace{A_{IN} v_{IN}^* \Delta t}^{\text{volume}}$$

$$\begin{aligned}
\Delta W_{IN} &= F \cdot distance \\
&= \underbrace{P_{IN} A_{IN}}_F \cdot \underbrace{v_{IN}^* \Delta t}_{\Delta s} \\
&= \frac{P_{IN} \Delta m_{IN}}{\rho_{IN}}
\end{aligned}$$

with

$$v = \frac{1}{\rho}$$

$$\Delta W_{IN} = (P v \Delta m)_{IN} \rightarrow \text{flow work} \quad (2)$$

Similarly

$$\Delta W_{OUT} = (P v \Delta m)_{OUT} \quad (3)$$

Substituting Eqs. 2 and 3 into Eq. 1 gives the 1st law for a control volume

$$\begin{aligned}
E_{CV}(t + \Delta t) - E_{CV}(t) &= \Delta Q + \Delta W_{shaft} + \Delta m_{IN}(e + Pv)_{IN} \\
&\quad - \Delta m_{OUT}(e + Pv)_{OUT}
\end{aligned} \quad (4)$$

Equation 4 can also be written as a rate equation \rightarrow divide through by Δt and take the limit as $\Delta t \rightarrow 0$

$$\frac{d}{dt} E_{CV} = \dot{Q} + \dot{W}_{shaft} + [\dot{m}(e + Pv)]_{IN} - [\dot{m}(e + Pv)]_{OUT}$$

where:

$$\dot{m} = \rho v^* A$$

Note that:

$$\begin{aligned}
e + Pv &= \underbrace{u + Pv} + \frac{(v^*)^2}{2} + gz \\
&= h(\text{enthalpy}) + KE + PE
\end{aligned}$$

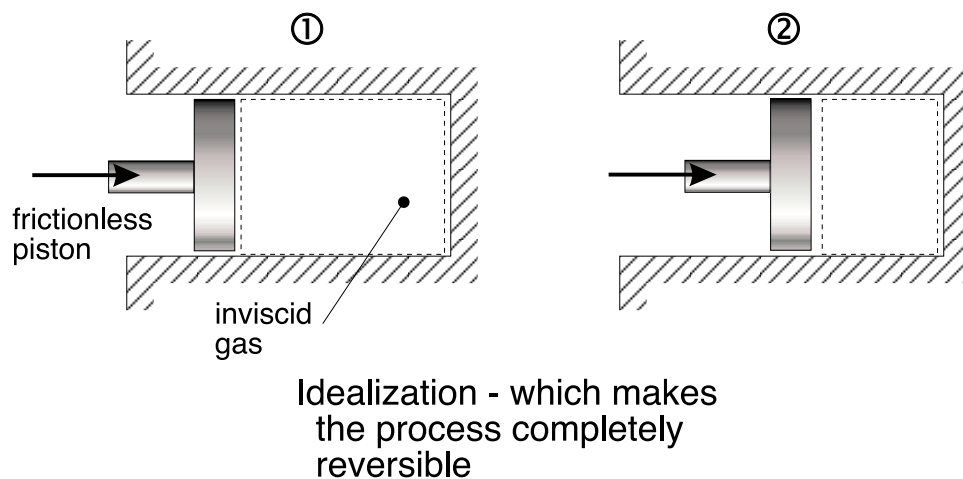
Second Law of Thermodynamics

1. *Entropy is a measure of the degree of microscopic disorder and represents our uncertainty about the microscopic state.*
2. The entropy of a system plus its surroundings (i.e. an isolated system) can never decrease (2nd law).

The second law states:

$$(\Delta S)_{system} + (\Delta S)_{surr.} \geq 0 \quad \text{where } \Delta \equiv \textit{final} - \textit{initial}$$

Example: Slow adiabatic compression of a gas



A process $1 \rightarrow 2$ is said to be reversible if the reverse process $2 \rightarrow 1$ restores the system to its original state without leaving any change in either the system or its surroundings.

\rightarrow idealization where $S_2 = S_1 \Rightarrow \mathcal{P}_S = 0$

$T_2 > T_1 \Rightarrow$ increased microscopic disorder

$V_2 < V_1 \Rightarrow$ reduced uncertainty about the whereabouts of molecules

Reversible + Adiabatic Process \Rightarrow Isentropic Process

The 2nd law states:

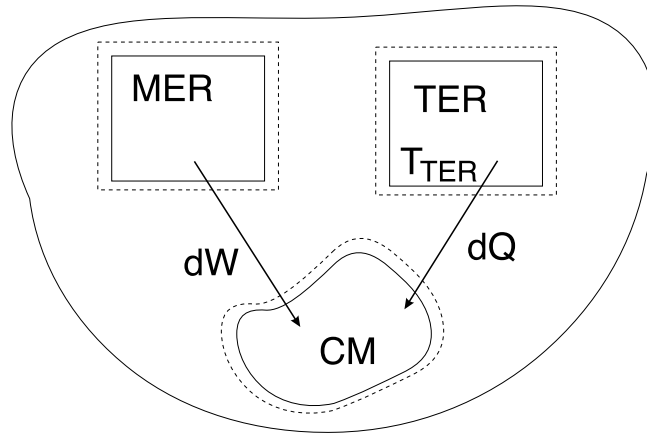
$$\mathcal{P}_S = (\Delta S)_{system} + (\Delta S)_{surr} \geq 0$$

where:

> 0 *irreversible (real world)*

$= 0$ *reversible (frictionless, perfectly elastic, inviscid fluid)*

How do we determine entropy in a system?



For an isolated system $\mathcal{P} \geq 0$.

$$(dS)_{CM} + \underbrace{(dS)_{TER}}_{-\frac{dQ}{T_{TER}}} + (dS^0)_{MER} = d\mathcal{P}_S$$

Therefore

$$(dS)_{CM} = \frac{dQ}{T_{TER}} + d\mathcal{P}_S$$

Integrating gives

$$(S_2 - S_1)_{CM} = \frac{Q_{1-2}}{T_{TER}} + \underbrace{\mathcal{P}_{S_{1-2}}}_{\geq 0}$$

where

$\frac{Q_{1-2}}{T_{TER}}$ - the entropy associated with heat transfer across a finite temperature difference

Gibb's Equation for a Simple Compressible Substance

simple \rightarrow has only one work mode

compressible \rightarrow the work mode is Pdv work

$$S = S(U, V)$$
$$dS = \underbrace{\left(\frac{\partial S}{\partial U}\right)_V}_{=\frac{1}{T}} dU + \underbrace{\left(\frac{\partial S}{\partial V}\right)_U}_P dV$$

$$\boxed{T dS = dU + P dV}$$

This form of Gibb's equation is very general and very useful.

The general derivation of Gibb's equation:

$$\text{from the 1st law} \Rightarrow dq = du + Pdv \quad (1)$$

$$\text{from the 2nd law} \Rightarrow ds = \frac{dq}{T} \quad (2)$$

Combining (1) and (2) gives

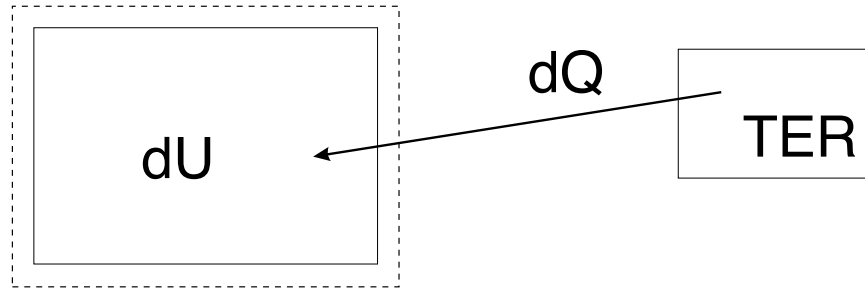
$$ds = \frac{du}{T} + P \frac{dv}{T}$$

or

$$T ds = du + P dv$$

$$T dS = dU + P dV$$

Second Law Analysis for a Control Mass



- control mass is uniformly at T_{TER} at all times
- control mass has a fixed size ($V = \textit{constant}$)

From Gibb's equation

$$T_{TER} dS = dU + P dV^0$$

From the 1st law

$$dU = dQ$$

Therefore for a reversible process

$$dS = \frac{dQ}{T_{TER}}$$

We integrate to give

$$S_2 - S_1 = \frac{Q_{1-2}}{T_{TER}}$$

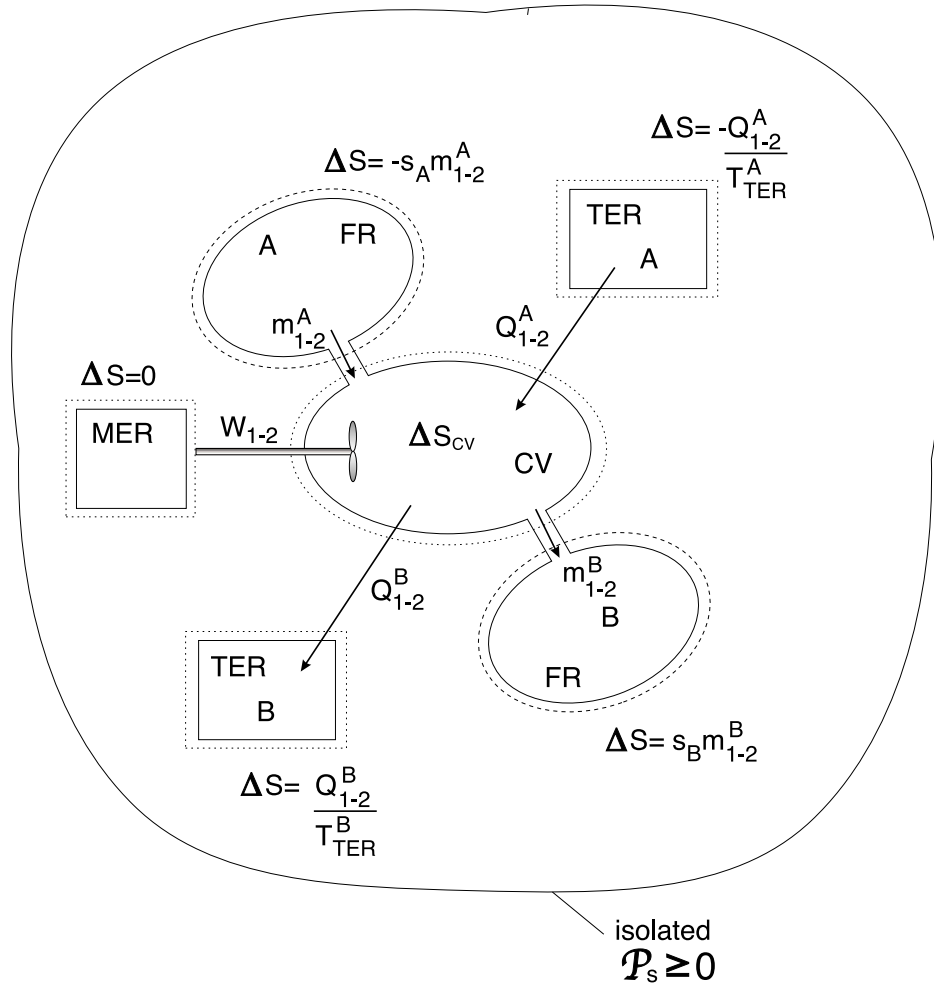
and for a non-reversible process

$$dS = \frac{dQ}{T_{TER}} + d\mathcal{P}_S$$

We integrate to give

$$S_2 - S_1 = \frac{Q_{1-2}}{T_{TER}} + \mathcal{P}_{S_{1-2}}$$

Second Law Analysis for a Control Volume



For the isolated system

$$(\Delta S)_{sys} + (\Delta S)_{sur} = \mathcal{P}_{S_{1-2}} \geq 0$$

$$\Delta S_{CV} - s_A m_{1-2}^A + s_B m_{1-2}^B - \frac{Q_{1-2}^A}{T_{TER}^A} + \frac{Q_{1-2}^B}{T_{TER}^B} = \mathcal{P}_{S_{1-2}}$$

or as a rate equation

$$\left(\frac{dS}{dt} \right)_{CV} = \left(s\dot{m} + \frac{\dot{Q}}{T_{TER}} \right)_{IN} - \left(s\dot{m} + \frac{\dot{Q}}{T_{TER}} \right)_{OUT} + \dot{\mathcal{P}}_S$$

This can be thought of as **accumulation** = **IN** - **OUT** + **generation**