

Review of First and Second Law of Thermodynamics



Reading

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Problems

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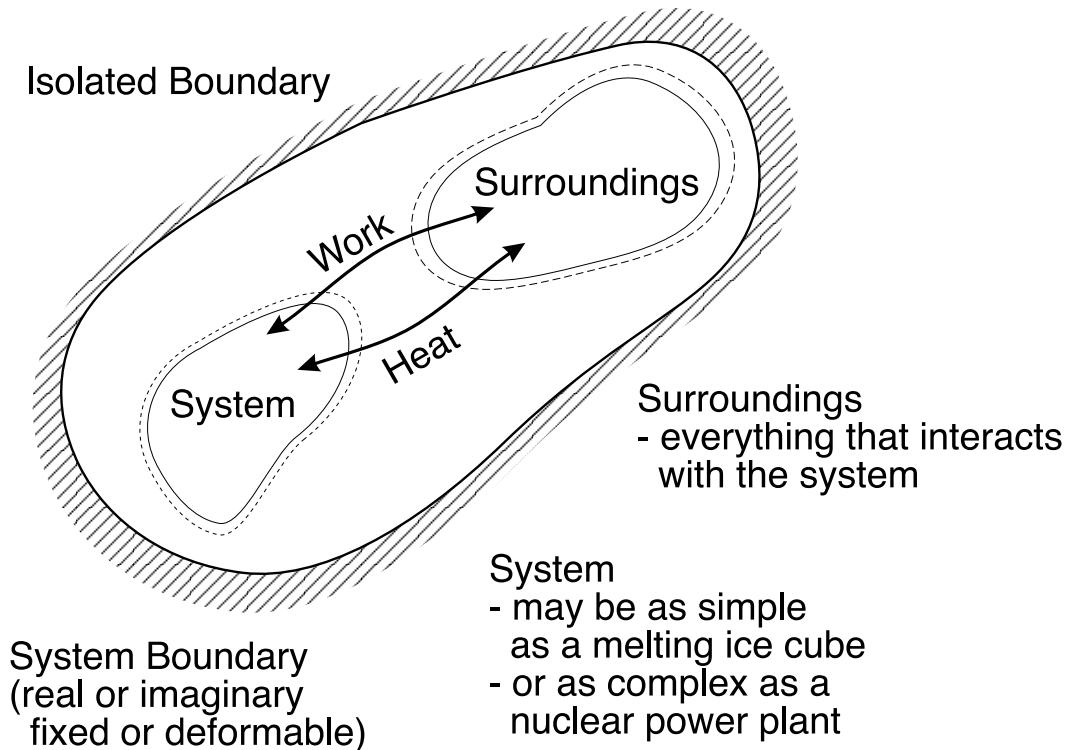
Definitions

SYSTEM:

- any specified collection of matter under study.
- all systems possess properties like mass, energy, entropy, volume, pressure, temperature, etc.

WORK & HEAT TRANSFER:

- thermodynamics deals with these properties of matter as a system interacts with its surroundings through work and heat transfer
- work and heat transfer are NOT properties → they are the forms that energy takes to cross the system boundary



First Law of Thermodynamics

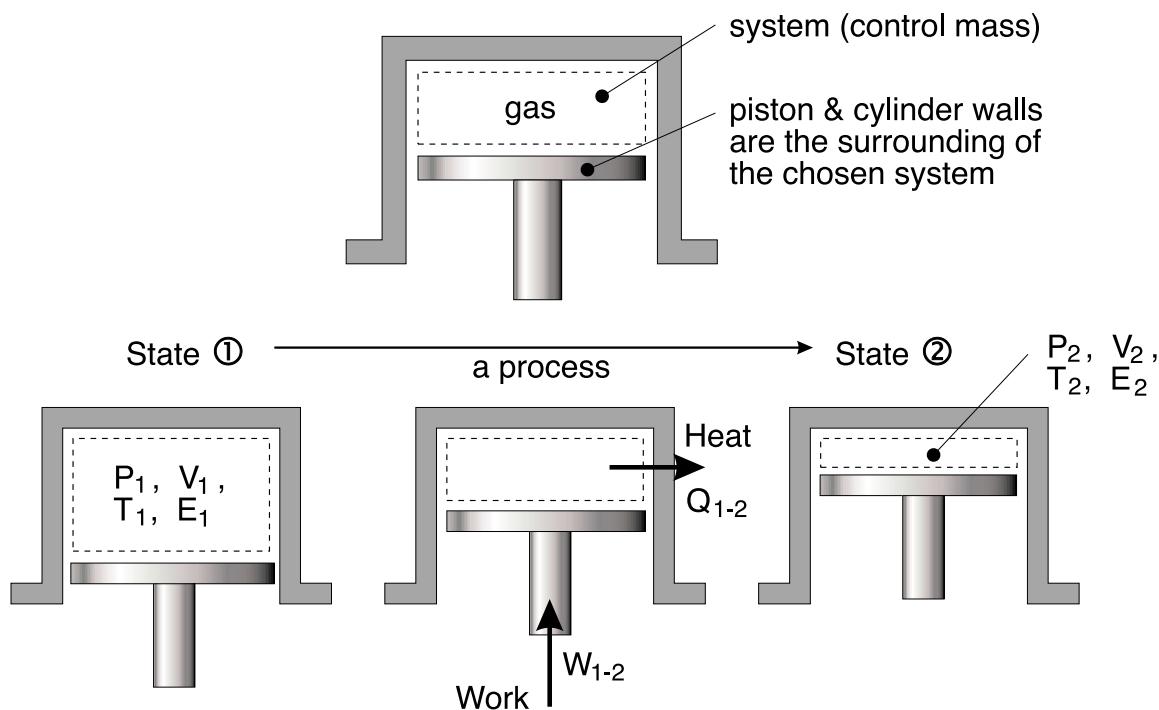
Control Mass (Closed System)

CONSERVATION OF ENERGY:

- the energy content of an isolated system is constant

$$\text{energy entering} - \text{energy leaving} = \text{change of energy within the system}$$

Example: A Gas Compressor



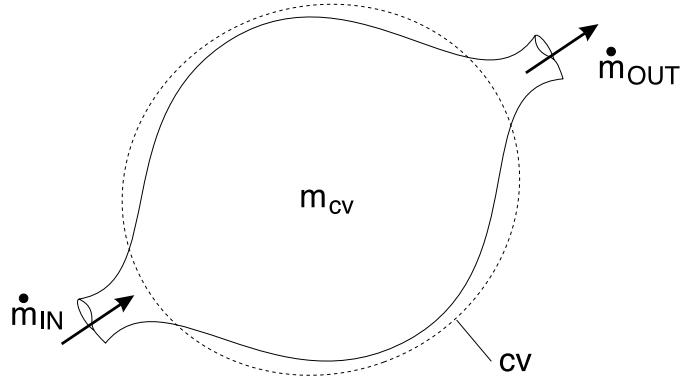
Performing a 1st law energy balance:

$$\left\{ \begin{array}{l} \text{Initial} \\ \text{Energy} \\ E_1 \end{array} \right\} + \left\{ \begin{array}{l} \text{Energy gain } W_{1-2} \\ \text{Energy loss } Q_{1-2} \end{array} \right\} = \left\{ \begin{array}{l} \text{Final} \\ \text{Energy} \\ E_2 \end{array} \right\}$$

$$E_1 + W_{1-2} - Q_{1-2} = E_2$$

Control Volume Analysis (Open System)

CONSERVATION OF MASS:



$$\left\{ \begin{array}{l} \text{rate of increase} \\ \text{of mass within} \\ \text{the CV} \end{array} \right\} = \left\{ \begin{array}{l} \text{net rate of} \\ \text{mass flow} \\ \text{IN} \end{array} \right\} - \left\{ \begin{array}{l} \text{net rate of} \\ \text{mass flow} \\ \text{OUT} \end{array} \right\}$$

$$\frac{d}{dt}(m_{CV}) = \dot{m}_{IN} - \dot{m}_{OUT}$$

where:

$$m_{CV} = \int_V \rho \, dV$$

$$\dot{m}_{IN} = (\rho \, v^* \, A)_{IN}$$

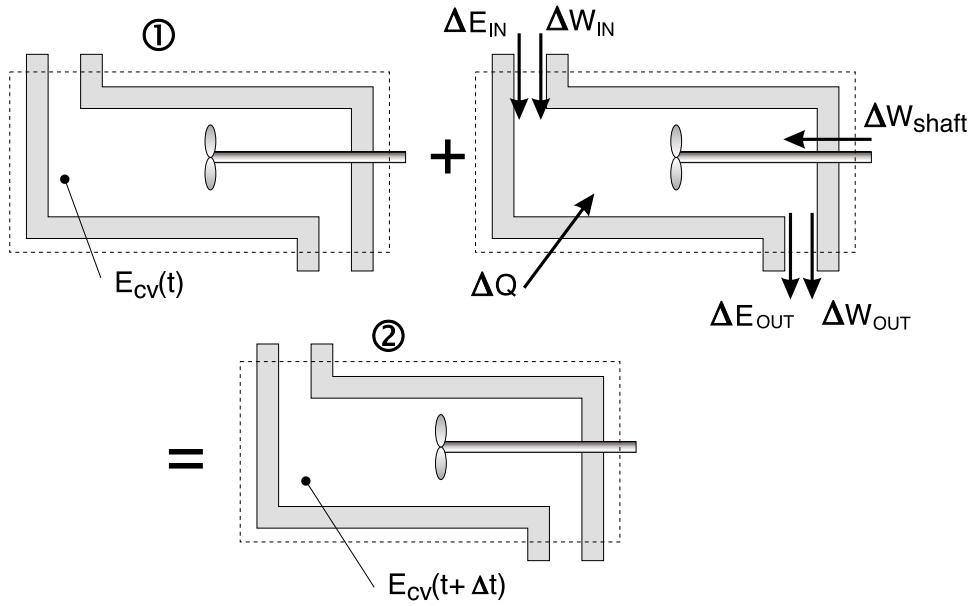
$$\dot{m}_{OUT} = (\rho \, v^* \, A)_{OUT}$$

with v^* = average velocity

CONSERVATION OF ENERGY:

The 1st law states:

$$\begin{aligned} E_{CV}(t) + \Delta Q + \Delta W_{shaft} + (\Delta E_{IN} - \Delta E_{OUT}) + \\ (\Delta W_{IN} - \Delta W_{OUT}) &= E_{CV}(t + \Delta t) \quad (1) \end{aligned}$$



where:

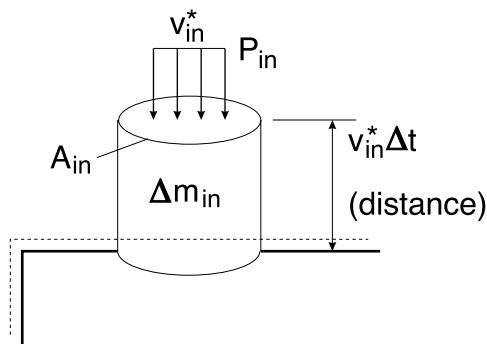
$$\Delta E_{IN} = e_{IN} \Delta m_{IN}$$

$$\Delta E_{OUT} = e_{OUT} \Delta m_{OUT}$$

$$\Delta W = \text{flow work}$$

$$e = \frac{E}{m} = \underbrace{\frac{u}{internal}}_{internal} + \underbrace{\frac{(v^*)^2}{2}}_{kinetic} + \underbrace{gz}_{potential}$$

What is flow work?



$$\Delta m_{IN} = \rho_{IN} \overbrace{A_{IN} v_{IN}^* \Delta t}^{volume}$$

$$\begin{aligned}
\Delta W_{IN} &= F \cdot \text{distance} \\
&= \underbrace{P_{IN} A_{IN}}_F \cdot \underbrace{v_{IN}^* \Delta t}_{\Delta s} \\
&= \frac{P_{IN} \Delta m_{IN}}{\rho_{IN}}
\end{aligned}$$

with

$$v = \frac{1}{\rho}$$

$$\Delta W_{IN} = (P v \Delta m)_{IN} \rightarrow \text{flow work} \quad (2)$$

Similarly

$$\Delta W_{OUT} = (P v \Delta m)_{OUT} \quad (3)$$

Substituting Eqs. 2 and 3 into Eq. 1 gives the 1st law for a control volume

$$\begin{aligned}
E_{CV}(t + \Delta t) - E_{CV}(t) &= \Delta Q + \Delta W_{shaft} + \Delta m_{IN}(e + Pv)_{IN} \\
&\quad - \Delta m_{OUT}(e + Pv)_{OUT}
\end{aligned} \quad (4)$$

Equation 4 can also be written as a rate equation \rightarrow divide through by Δt and take the limit as $\Delta t \rightarrow 0$

$$\frac{d}{dt} E_{CV} = \dot{Q} + \dot{W}_{shaft} + [\dot{m}(e + Pv)]_{IN} - [\dot{m}(e + Pv)]_{OUT}$$

where:

$$\dot{m} = \rho v^* A$$

Note that:

$$\begin{aligned}
e + Pv &= \underbrace{u + Pv}_{\text{enthalpy}} + \frac{(v^*)^2}{2} + gz \\
&= h(\text{enthalpy}) + KE + PE
\end{aligned}$$

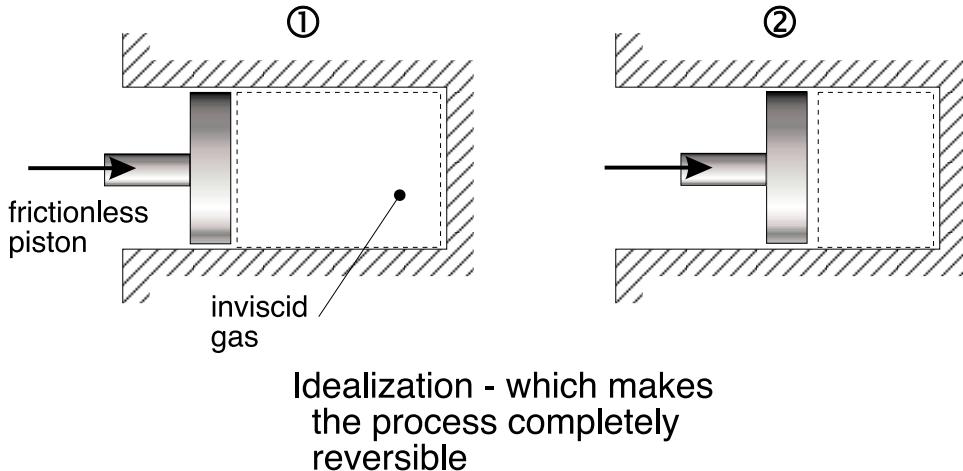
Second Law of Thermodynamics

1. Entropy is a measure of the degree of microscopic disorder and represents our uncertainty about the microscopic state.
2. The entropy of a system plus its surroundings (i.e. an isolated system) can never decrease (2nd law).

The second law states:

$$(\Delta S)_{\text{system}} + (\Delta S)_{\text{surr.}} \geq 0 \quad \text{where } \Delta \equiv \text{final} - \text{initial}$$

Example: Slow adiabatic compression of a gas



A process $1 \rightarrow 2$ is said to be reversible if the reverse process $2 \rightarrow 1$ restores the system to its original state without leaving any change in either the system or its surroundings.

→ idealization where $S_2 = S_1 \Rightarrow \mathcal{P}_S = 0$

$T_2 > T_1 \Rightarrow$ increased microscopic disorder

$V_2 < V_1 \Rightarrow$ reduced uncertainty about the whereabouts of molecules

Reversible + Adiabatic Process \Rightarrow Isentropic Process

The 2nd law states:

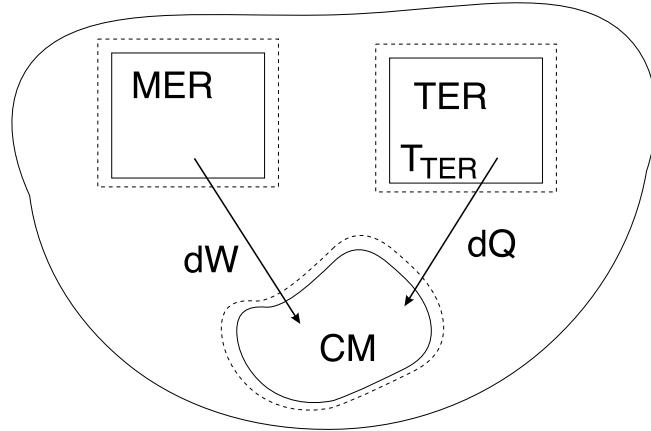
$$\mathcal{P}_S = (\Delta S)_{\text{system}} + (\Delta S)_{\text{surr}} \geq 0$$

where:

> 0 *irreversible (real world)*

$= 0$ *reversible (frictionless, perfectly elastic, inviscid fluid)*

How do we determine entropy in a system?



For an isolated system $\mathcal{P} \geq 0$.

$$(dS)_{CM} + \underbrace{(dS)_{TER}}_{-\frac{dQ}{T_{TER}}} + (dS^0)_{MER} = d\mathcal{P}_S$$

Therefore

$$(dS)_{CM} = \frac{dQ}{T_{TER}} + d\mathcal{P}_S$$

Integrating gives

$$(S_2 - S_1)_{CM} = \frac{Q_{1-2}}{T_{TER}} + \underbrace{\mathcal{P}_{S_{1-2}}}_{\geq 0}$$

where

$\frac{Q_{1-2}}{T_{TER}}$ - the entropy associated with heat transfer across a finite temperature difference

Gibb's Equation for a Simple Compressible Substance

simple \rightarrow has only one work mode

compressible \rightarrow the work mode is PdV work

$$S = S(U, V)$$

$$dS = \underbrace{\left(\frac{\partial S}{\partial U}\right)_V}_{= \frac{1}{T}} dU + \underbrace{\left(\frac{\partial S}{\partial V}\right)_U}_{= \frac{P}{T}} dV$$

$$\boxed{T dS = dU + PdV}$$

This form of Gibb's equation is very general and very useful.

The general derivation of Gibb's equation:

from the 1st law $\Rightarrow dq = du + Pdv$ (1)

from the 2nd law $\Rightarrow ds = \frac{dq}{T}$ (2)

Combining (1) and (2) gives

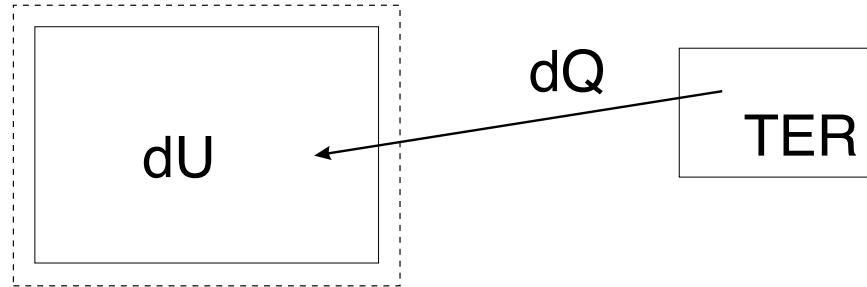
$$ds = \frac{du}{T} + P \frac{dv}{T}$$

or

$$T ds = du + P dv$$

$$T dS = dU + P dV$$

Second Law Analysis for a Control Mass



- control mass is uniformly at T_{TER} at all times
- control mass has a fixed size ($V = \text{constant}$)

From Gibb's equation

$$T_{TER} dS = dU + P dV^0$$

From the 1st law

$$dU = dQ$$

Therefore for a reversible process

$$dS = \frac{dQ}{T_{TER}}$$

We integrate to give

$$S_2 - S_1 = \frac{Q_{1-2}}{T_{TER}}$$

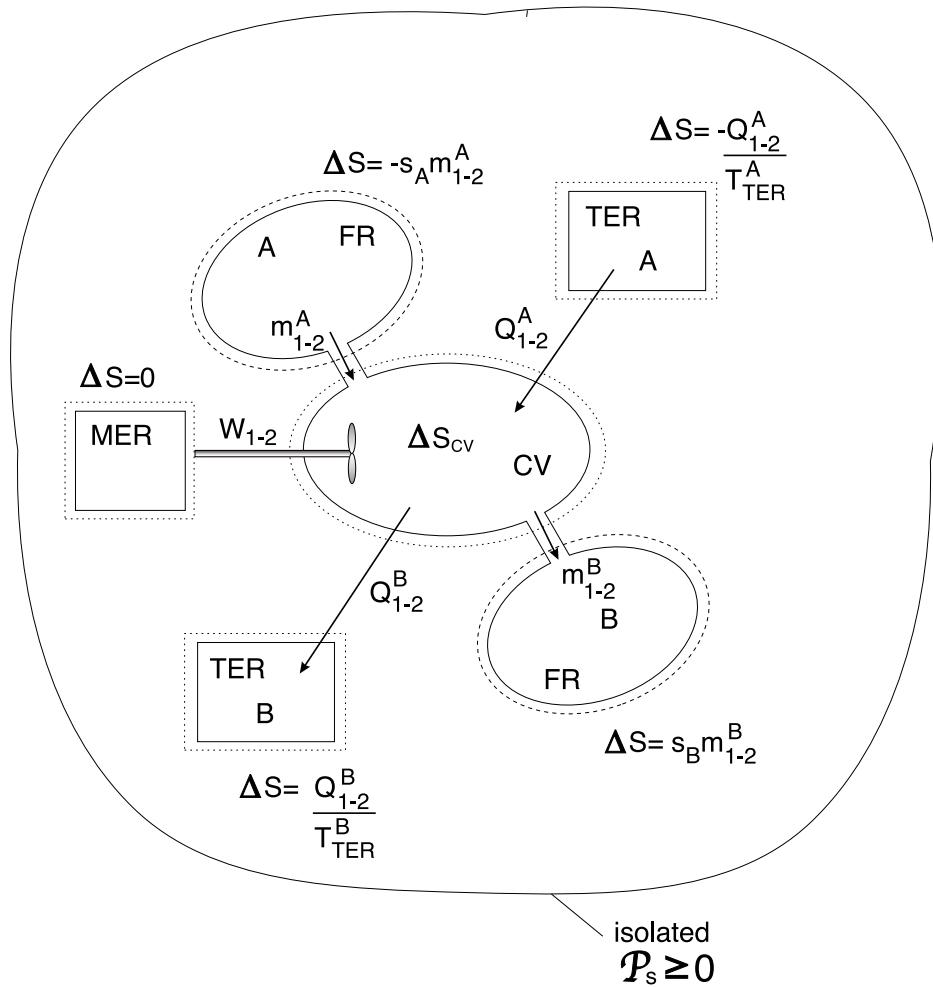
and for a non-reversible process

$$dS = \frac{dQ}{T_{TER}} + dP_S$$

We integrate to give

$$S_2 - S_1 = \frac{Q_{1-2}}{T_{TER}} + P_{S_{1-2}}$$

Second Law Analysis for a Control Volume



For the isolated system

$$(\Delta S)_{sys} + (\Delta S)_{sur} = \mathcal{P}_{S_{1-2}} \geq 0$$

$$\Delta S_{cv} - s_A m_{1-2}^A + s_B m_{1-2}^B - \frac{Q_{1-2}^A}{T_{TER}^A} + \frac{Q_{1-2}^B}{T_{TER}^B} = \mathcal{P}_{S_{1-2}}$$

or as a rate equation

$$\left(\frac{dS}{dt} \right)_{cv} = \left(s \dot{m} + \frac{\dot{Q}}{T_{TER}} \right)_{IN} - \left(s \dot{m} + \frac{\dot{Q}}{T_{TER}} \right)_{OUT} + \dot{\mathcal{P}}_s$$

This can be thought of as **accumulation = IN - OUT + generation**