

# Non-Reacting Gas Mixtures



## Reading

12-1 → 12-3

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## Problems

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## Introduction

- homogeneous gas mixtures are frequently treated as a single compound rather than many individual constituents
- the individual properties of inert gases tend to be submerged, such that the gas behaves as a single pure substance
- equations can be derived to express the properties of mixtures in terms of the properties of their individual constituents

## Formulations

- the total mass of a mixture,  $m$  is the sum of the masses of its components

$$m = m_1 + m_2 + \dots + m_j = \sum_{i=1}^j m_i$$

- the relative amounts of the components present in the mixture can be specified in terms of mass fractions

$$Y_i = \frac{m_i}{m} \quad \Rightarrow \quad \sum_{i=1}^j Y_i = 1$$

- the total number of moles in a mixture,  $n$  is the sum of the number of moles of each of the components

$$n = n_1 + n_2 + \dots + n_j = \sum_{i=1}^j n_i$$

- the relative amounts of the components present in the mixture can be specified in terms of mole fractions

$$X_i = \frac{n_i}{n} \quad \Rightarrow \quad \sum_{i=1}^j X_i = 1$$

- $m_1$  and  $n_i$  are related by the molecular weight  $\tilde{M}_i$

$$m_i = n_i \tilde{M}_i$$

Therefore the total mass is

$$m = \sum_{i=1}^j n_i \tilde{M}_i$$

- the mixture molecular weight can be calculated as a mole fraction average of the component molecular weights

$$\tilde{M} = \frac{m}{n} = \frac{\sum_{i=1}^j n_i \tilde{M}_i}{n} = \sum_{i=1}^j X_i \tilde{M}_i$$

- $X_i$  and  $Y_i$  are also related by the molecular weights

$$\frac{Y_i}{X_i} = \frac{(m_i/m)}{(n_i/n)} = \left( \frac{m_i}{n_i} \right) \left( \frac{n}{m} \right) = (\tilde{M}_i) \left( \frac{1}{\tilde{M}} \right)$$

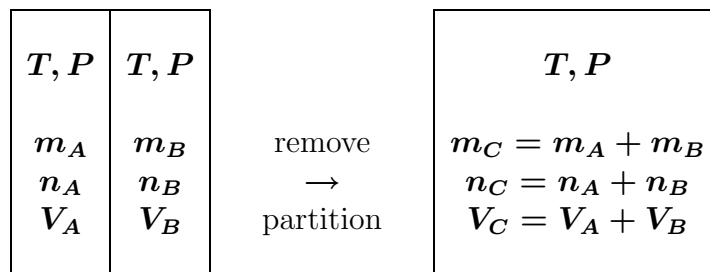
Therefore

$$\frac{Y_i}{X_i} = \frac{\tilde{M}_i}{\tilde{M}} \quad \rightarrow \quad Y_i = X_i \left[ \frac{\tilde{M}_i}{\sum_{i=1}^j X_i \tilde{M}_i} \right]$$

## P-V-T Relationships for Ideal Gas Mixtures

### Amagat Model (law of additive volumes)

- the volume of a mixture is the sum of the volumes that each constituent gas would occupy if each were at the pressure,  $P$  and temperature,  $T$ , of the mixture



*The volume of the gas mixture is equal to the sum of the volumes each gas would occupy if it existed at the mixture temperature and pressure.*

$$V = \sum_{i=1}^j V_i$$

### Dalton Model (law of additive pressures)

- the pressure of a mixture of gases is the sum of the pressures of its components when each alone occupies the volume of the mixture,  $V$ , at the temperature,  $T$ , of the mixture

$$\begin{array}{|c|} \hline V, T \\ \hline m_A, n_A, P_A \\ \hline \end{array} + \begin{array}{|c|} \hline V, T \\ \hline m_B, n_B, P_B \\ \hline \end{array} = \begin{array}{|c|} \hline V, T \\ \hline m_C = m_A + m_B \\ n_C = n_A + n_B \\ P_C = P_A + P_B \\ \hline \end{array}$$

*The pressure of a gas mixture is equal to the sum of the pressures each gas would exert if it existed alone at  $T$  and  $V$ .*

By combining the results of the Amagat and Dalton models i.e. (1) and (2), we obtain

$$\frac{P_i}{P} = \frac{V_i}{V} = \frac{n_i}{n}$$

Therefore, Amagat's law and Dalton's law are equivalent to each other if the gases and the mixture are ideal gases.

## Mixture Properties

Extensive properties such as  $\mathbf{U}$ ,  $\mathbf{H}$ ,  $\mathbf{c}_p$ ,  $\mathbf{c}_v$  and  $\mathbf{S}$  can be found by adding the contribution of each component at the condition at which the component exists in the mixture.

$$\begin{aligned} U = \sum U_i &= \sum m_i u_i = m \sum Y_i u_i = m u \\ &= \sum n_i \bar{u}_i = n \sum X_i \bar{u}_i = n \bar{u} \end{aligned}$$

where  $\bar{u}$  is the specific internal energy of the mixture per mole of the mixture.

$u = \sum Y_i u_i$
$h = \sum Y_i h_i$
$c_v = \sum Y_i c_{v_i}$
$c_p = \sum Y_i c_{p_i}$
$s = \sum Y_i s_i$

Changes in internal energy and enthalpy of mixtures

$$u_2 - u_1 = \sum Y_i (u_2 - u_1)_i = \int_{T_1}^{T_2} c_v dT = c_v (T_2 - T_1)$$

$$h_2 - h_1 = \sum Y_i (h_2 - h_1)_i = \int_{T_1}^{T_2} c_p dT = c_p (T_2 - T_1)$$

$$s_2 - s_1 = \sum Y_i (s_2 - s_1)_i = c_p \ln \frac{T_2}{T_1} - R \ln \frac{P_2}{P_1}$$

These relationships can also be expressed on a per mole basis.

## Entropy Change Due to Mixing of Ideal Gases

- when ideal gases are mixed, a change in entropy occurs as a result of the increase in disorder in the systems
- if the initial temperature of all constituents are the same and the mixing process is adiabatic
  - temperature does not change
  - but entropy does

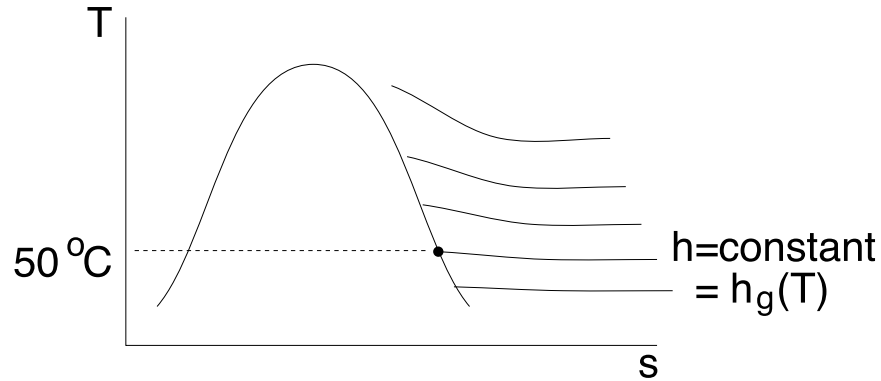
$$\begin{aligned}\Delta S &= - \left( m_A R_A \ln \frac{P_A}{P} + m_B R_B \ln \frac{P_B}{P} + \cdots \right) \\ &= - \sum_{i=1}^j m_i R_i \ln \frac{P_i}{P} \\ &= - \mathcal{R} \sum_{i=1}^j n_i \ln X_i\end{aligned}$$

Notes:

- -ve sign because  $\ln \frac{P_i}{P} < 0$
- $m_i R_i = m_i \frac{\mathcal{R}}{\tilde{M}_i} = n_i \mathcal{R}$

# Psychrometrics

- studies involving mixtures of dry air and water vapour
- for  $T \leq 50^\circ\text{C}$  ( $P_{sat} \leq 13 \text{ kPa}$ )  $\Rightarrow h \approx h(T)$ 
  - water vapour can be treated as an ideal gas



## Definitions

### Moist Air

- a mixture of dry air and water vapour where dry air is treated as if it were a pure component
- the overall mixture is given as  $\Rightarrow P = \frac{mRT}{V}$

### Total Pressure

$$P = P_a + P_w$$

$$P_a = \frac{m_a R_a T}{V}$$

$$P_w = \frac{m_w R_w T}{V}$$

where  $P_a$  is the partial pressure of air and  $P_w$  is the partial pressure of water vapour. Typically  $m_w \ll m_a$ .

### Relative Humidity - $\phi$

$$\phi = \frac{P_w(T)}{P_{sat}(T)} = \frac{\text{vapour pressure at the prevailing T}}{\text{saturation pressure at the prevailing T}}$$

If  $P_w = P_{sat}(T)$  the mixture is said to be saturated.

The relative humidity can also be written as

$$\phi = \frac{P_w}{P_{sat}} = \frac{\rho_w}{\rho_{sat}} = \frac{v_g}{v_w} = \frac{\text{mixture volume}}{\text{water volume}}$$

where  $v_g$  is the mixture specific volume and  $v_w$  is water specific volume.

### Specific Humidity (Humidity ratio) - $\omega$

$$\begin{aligned}\omega &= \frac{m_w}{m_a} = \frac{\text{mass of water vapour}}{\text{mass of air}} \\ &= \frac{\tilde{M}_w n_w}{\tilde{M}_a n_a} = \frac{\tilde{M}_w (P_w V / \mathcal{R}T)}{\tilde{M}_a (P_a V / \mathcal{R}T)} \\ &= \left( \frac{\tilde{M}_w}{\tilde{M}_a} \right) \left( \frac{P_w}{P_a} \right) \\ &= 0.622 \left( \frac{P_w}{P_a} \right)\end{aligned}$$

In addition  $\omega$  can be written as

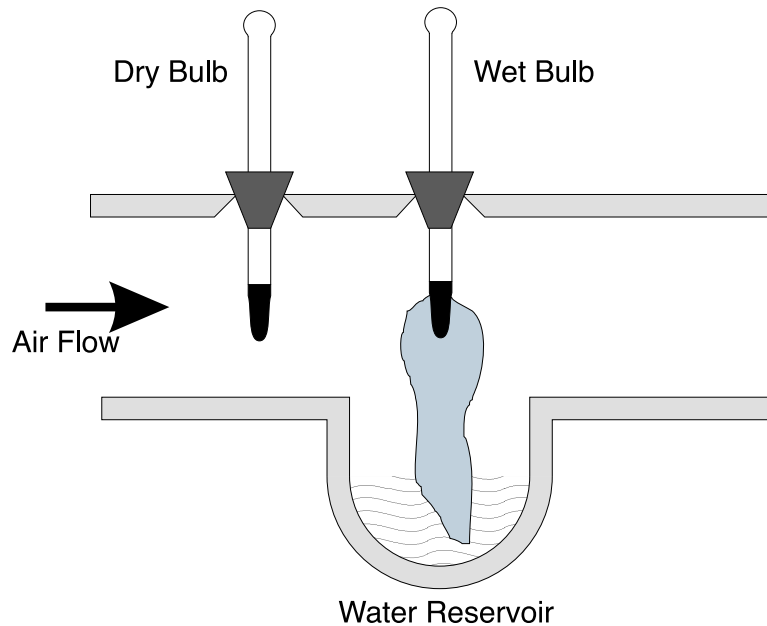
$$\omega = 0.622 \left( \frac{P_w}{P_a} \right) = 0.622 \left( \frac{P_w}{P - P_w} \right) = 0.622 \left( \frac{\phi P_{sat}}{P - \phi P_{sat}} \right)$$

which can be rearranged in terms of relative humidity

$$\phi = \frac{P \gamma}{P_{sat} \left( \omega + \frac{\tilde{M}_w}{\tilde{M}_a} \right)} = \frac{P \omega}{P_{sat} (\omega + 0.622)}$$

**Dry Bulb Temperature** - the temperature measured by a thermometer placed in a mixture of air and water vapour

**Wet Bulb Temperature**

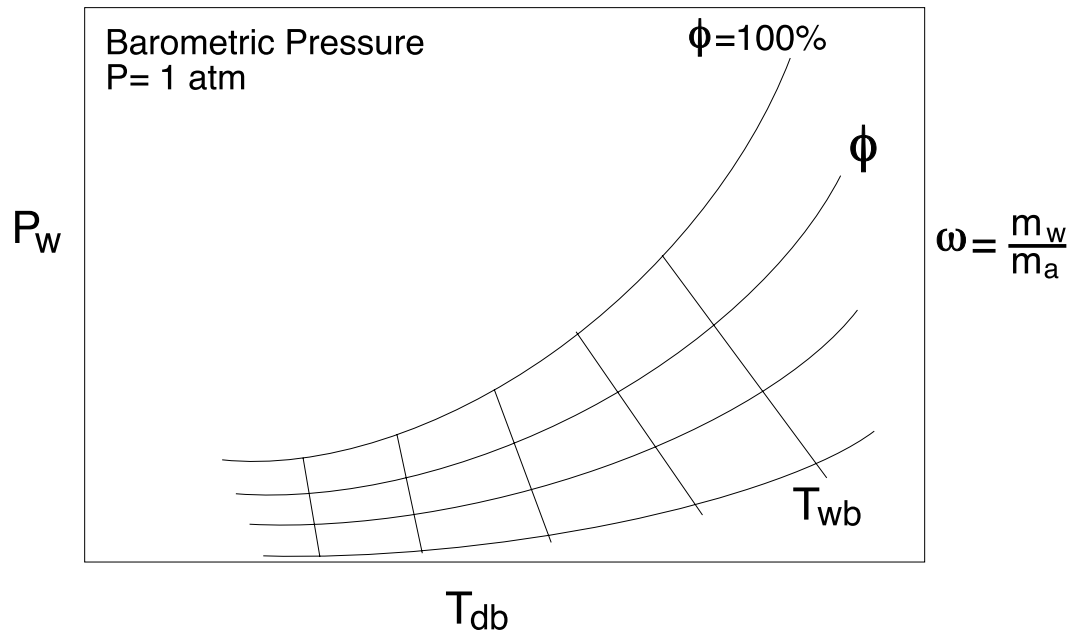


- thermometer surrounded by a saturated wick
- if air/water vapour mixture is not saturated, some water in the wick evaporates and diffuses into the air → cooling the water in the wick
- at the temperature of the water drops, heat is transferred to the water from both the air and the thermometer
- the steady state temperature is the wet-bulb temperature

**Sling Thermometer** - a rotating set of thermometers one of which measures wet bulb temperature and the other dry bulb temperature.  $T_{DB}$  and  $T_{WB}$  are sufficient to fix the state of the mixture.



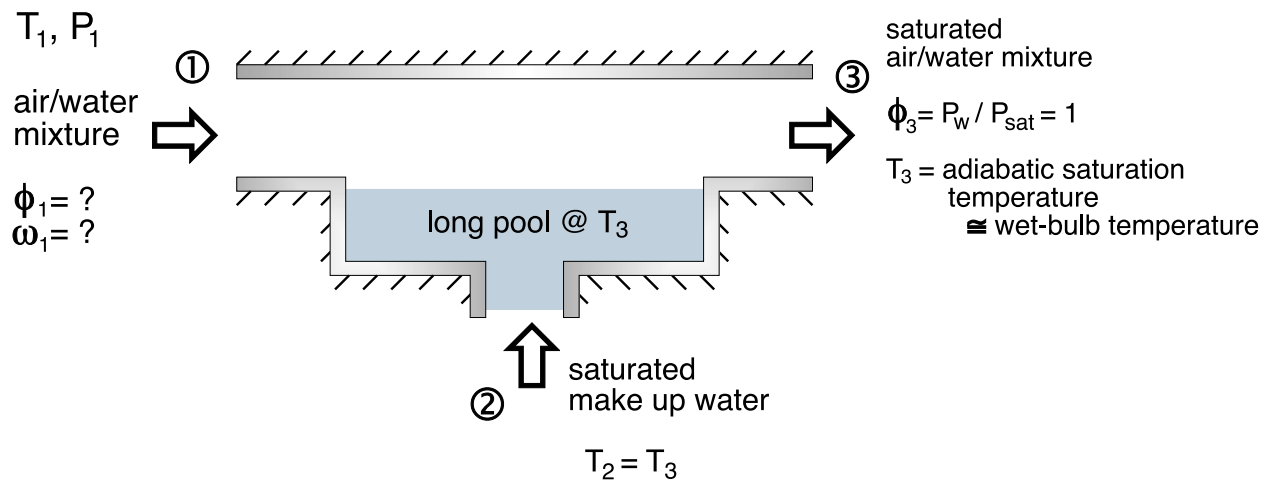
# The Psychrometric Chart



where the **dry bulb** temperature is the temperature measured by a thermometer place in the mixture and the **wet bulb** temperature is the adiabatic saturation temperature.

## An Adiabatic Saturator

How can we measure humidity?



- the adiabatic saturator is used to measure humidity

- two inlets, single exit device through which moist air passes
- air-water mixture of unknown humidity enters at a known pressure and temperature
- if air/water mixture is not saturated, ( $\phi < 100\%$ ), some water from the pool will evaporate
- the energy required to evaporate the water comes from the moist air  $\rightarrow$  mixture temperature decreases
- for a sufficiently long duct, the moisture exits with  $\phi_3 = 1$
- the temperature of the exiting mixture is called the adiabatic saturation temperature